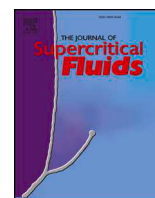




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## Application of Quality by Design to the robust preparation of a liposomal GLA formulation by DELOS-susp method

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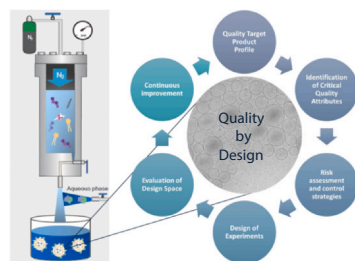
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## HIGHLIGHTS

- Robust preparation of liposomal formulation by DELOS-susp method.
- Implementation of Quality by Design methodology to liposomes preparation.
- Influence of critical parameters on quality was studied through DoE analysis.
- Design Space was obtained for GLA-loaded liposomes formulation.

## GRAPHICAL ABSTRACT



**Abbreviations:** BCA, Bicinchoninic acid assay; Chol, Cholesterol; Chol-PEG<sub>400</sub>-RGD, Cholesterol pegylated with arginyl-glycyl-aspartic (RGD) acid peptide; CMA, Critical Material Attributes; CO<sub>2</sub>, Carbon dioxide; CoA, Certificate of Analysis; CPP, Critical Process Parameters; CQA, Critical Quality Attribute; Cryo-TEM, Cryogenic Transmission Electron Microscopy; DELOS-susp, Depressurization of an Expanded Liquid Organic Solution into aqueous solution; DLS, Dynamic Light Scattering; DMSO, Dimethyl sulfoxide; DoE, Design of Experiments; DPPC, 1,2-Dipalmitoyl-sn-glycero-3-phosphocholine; EA, Enzymatic Activity; EE, Entrapment Efficiency; EHS, Environment, Health and Safety; EMA, European Medicines Agency; ERT, Enzyme Replacement Therapy; EtOH, Ethanol; FDA, Food and Drug Administration;  $f_{\text{single}}$ , Ratio of monolayered liposomes; GLA,  $\alpha$ -galactosidase A enzyme; H<sub>2</sub>O, Water; HPLC, High Performance Liquid Chromatography; ICH, Council for Harmonisation of Technical Requirements for Pharmaceuticals for Human Use; LSD, Lysosomal storage disorders; MKC, Myristalkonium chloride; N<sub>2</sub>, Nitrogen; nanoGLA, GLA-loaded nanoliposomes; NTA, Nanoparticle Tracking Analysis; PEG, Polyethylene Glycol; PLS, Partial Least Squares; PdI, Polydispersity Index; PIC, Pressure Indicator Controller; Pw, Working pressure; QbD, Quality by Design; RGD, Arginine-Glycine-Aspartic acid; SAXS, Small-Angle X-ray Scattering; SbD, Safe by Design; SDS-PAGE, Sodium Dodecyl Sulfate Polyacrylamide Gel Electrophoresis; S-MLS, Static Multiple Light Scattering; TFF, Tangential Flow Filtration; TGX, Trys-Glycine eXtended; TIC, Temperature Indicator Controller; TSI, Turbiscan Stability Index; Tw, Working temperature; USP, United States Pharmacopeia; X<sub>CO<sub>2</sub></sub>, Carbon dioxide molar fraction

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## ABSTRACT

Fabry disease is a lysosomal storage disease arising from a deficiency of the enzyme  $\alpha$ -galactosidase A (GLA). The enzyme deficiency results in an accumulation of glycolipids, which over time, leads to cardiovascular, cerebrovascular, and renal disease, ultimately leading to death in the fourth or fifth decade of life. Currently, lysosomal storage disorders are treated by enzyme replacement therapy (ERT) through the direct administration of the missing enzyme to the patients.

In view of their advantages as drug delivery systems, liposomes are increasingly being researched and utilized in the pharmaceutical, food and cosmetic industries, but one of the main barriers to market is their scalability.

Depressurization of an Expanded Liquid Organic Solution into aqueous solution (DELOS-susp) is a compressed fluid-based method that allows the reproducible and scalable production of nanovesicular systems with remarkable physicochemical characteristics, in terms of homogeneity, morphology, and particle size. The objective of this work was to optimize and reach a suitable formulation for in vivo preclinical studies by implementing a Quality by Design (QbD) approach, a methodology recommended by the FDA and the EMA to develop robust drug manufacturing and control methods, to the preparation of  $\alpha$ -galactosidase-loaded nanoliposomes (nanoGLA) for the treatment of Fabry disease.

Through a risk analysis and a Design of Experiments (DoE), we obtained the Design Space in which GLA concentration and lipid concentration were found as critical parameters for achieving a stable nanoformulation. This Design Space allowed the optimization of the process to produce a nanoformulation suitable for in vivo preclinical testing.

## 1. Introduction

One of the main challenges to produce advanced materials such as enzyme-loaded liposomes is the successful implementation of new manufacturing nanotechnologies at industrial scale. The DELOS-susp method is a compressed fluid-based technology that allows the reproducible preparation of different nanovesicular systems with remarkable physicochemical characteristics, in terms of homogeneity, morphology and particle size, as well as a high versatility to integrate different active compounds, that can lead to innovative nanomedicines with enhanced efficiency [1–3].

Lysosomal storage disorders (LSD) are diseases caused by lysosomal dysfunction usually as a consequence of deficiency of a single metabolic enzyme. In the case of Fabry disease, the lack of  $\alpha$ -galactosidase A (GLA) enzyme causes the accumulation of glycosphingolipids leading to multiple organ pathology [4]. Enzyme replacement therapy (ERT), which is the main current treatment, exhibits several drawbacks mainly related to protein instability and low efficacy [5].

To overcome the main limitations of the current ERTs (e.g. rapid enzyme degradation, high immunogenicity, short circulation half-life, poor biodistribution, and limited efficacy among others [6]) a strategy under development consists in the encapsulation of the GLA enzyme into nanoliposomes. Such encapsulation aims to protect the enzyme, decrease the degradation and immunogenicity of GLA, and increase its plasma half-life. Moreover, the addition of a targeting peptide on the liposomal membrane can facilitate cellular up-take via peptide receptors recognition and could help to improve GLA biodistribution. Thus, GLA-loaded nanoliposomes (nanoGLA) functionalized with Arginine-Glycine-Aspartic acid (RGD) peptide and prepared by DELOS-susp, have recently been reported to increase enzymatic activity and intracellular penetration, showing the great potential of this CO<sub>2</sub>-based methodology for the simple production of protein-nanoliposome therapeutic conjugates [4,7]. Fig. 1 shows the DELOS-susp process and the starting materials used to obtain the nanoGLA liposomal formulation.

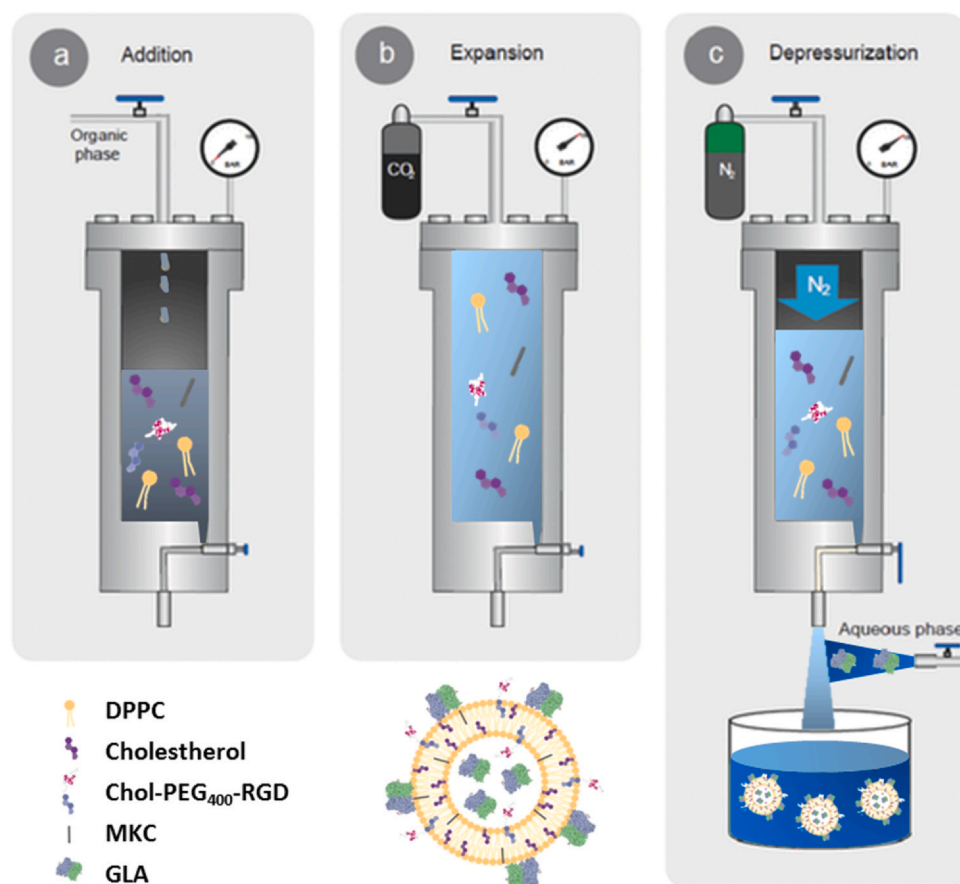
The results obtained in earlier stages of nanoGLA development, although being biocompatible and showing interesting in vitro activity, presented some limitations regarding formulation characteristics for continuing with their translation towards the clinics. In first place, the concentration of GLA enzyme we could load into the nanoliposomes, with robust particle size and PDI, was around 20  $\mu$ g/mL, far below the minimum required for reaching those doses that will allow to perform

efficacy studies in mice (200  $\mu$ g/mL). Besides, the enzyme entrapment efficiency in the liposomes was below 40% [4]. The addition of cationic surfactant myristalkonium chloride (MKC) into the formulation in low concentration allowed to increase the drug entrapment efficiency as well as the colloidal stability of the system [7]. However, further work was required in order to obtain a stable formulation with the proper protein concentration.

In this work we applied the Quality by Design (QbD) approach to determine formulation and process parameters that could have an important impact on nanoGLA attributes when prepared by DELOS-susp. The QbD methodology is described in Guidelines of the International Council for Harmonisation of Technical Requirements for Pharmaceuticals for Human Use (ICH) [8–10] and it is strongly encouraged by the Food and Drug Administration (FDA) and the European Medicines Agency (EMA) to develop robust drug manufacturing and control methods. Pharmaceutical QbD is a systematic approach to development that aims to ensure the quality of medicines, identifying characteristics that are critical to quality from the patient's perspective, translating them into the product Critical Quality Attributes (CQAs), and establishing a relationship between manufacturing variables and CQAs through a Design of Experiments (DoE). The goals of the pharmaceutical QbD may include the achievement of meaningful product quality specifications as well as the reduction of product variability and defects, to increase efficiencies and to enhance root cause analysis [11].

Another systematic methodology used in pharmaceutical design is the Safe by Design (SbD) approach, which aims to eliminate possible risks to the human health and the environment at early innovation stages, i.e., during the design or planning stage [12]. SbD requires a full life cycle perspective combined with nanomaterial sustainability (environmental, social, and economic) [13] improvements, to avoid the shifting of potential risks across development stages.

In this framework, we report here the implementation of the QbD approach to develop a robust process for the preparation of nanoGLA. In the present work, the process was scaled-up from previous work [4] by a 7-fold factor, and the liposomal prototype was optimized increasing 10-times (i.e. from around 20 to 200  $\mu$ g/mL) the final concentration of GLA enzyme in the nanoformulation. Its physicochemical stability was improved while meeting the defined quality specifications in order to fulfill the required therapeutic doses for advanced preclinical testing. Besides, a SbD evaluation of the nanoGLA manufacturing process by DELOS-susp is also presented.



**Fig. 1.** Schematic representation of the DELOS-susp method for the preparation of GLA loaded nanoliposomes (nanoGLA). The procedure includes: a) Loading of an organic solution containing the liposome membrane components (Cholesterol, DPPC, Cholesterol-PEG<sub>400</sub>-RGD, MKC) into the high pressure vessel; b) Addition of compressed CO<sub>2</sub> until a certain pressure to produce a CO<sub>2</sub>-expanded solution, where all membrane components remain dissolved in a single liquid phase; and c) Depressurization of the expanded solution over an aqueous solution containing the GLA enzyme at atmospheric pressure, obtaining the protein-liposomes nanoconjugates. Figure adapted from [4].

## 2. Materials and methods

### 2.1. Materials

GLAcmycHis protein (GLA) was synthesized as explained in [Appendix A](#). 1,2-Dipalmitoyl-sn-glycero-3-phosphocholine (DPPC) was purchased from Cordem Pharma (Liestal, Switzerland), cholesterol was purchased from Panreac Química (Castellar del Vallès, Spain), and myristalkonium chloride (MKC) from United States Biological (Salem, US). Cholesterol pegylated with arginyl-glycyl-aspartic acid peptide (Chol-PEG<sub>400</sub>-RGD) was synthesized as described by E. Cristóbal-Lecina et al. [14]. Ethanol (EtOH) was purchased from Scharlab (Sentmenat, Spain), dimethyl sulfoxide (DMSO) from Sigma-Aldrich (St. Louis, US), carbon dioxide (CO<sub>2</sub>) and nitrogen (N<sub>2</sub>) from Carburros Metálicos (Cornellà de Llobregat, Spain). Diafiltration column modules of 300 kDa cut-off were purchased from Repligen (Waltham, US). Ultrapure Type I water (H<sub>2</sub>O), purified using Milli-Q Advantage A10 equipment from Millipore Corporation (Burlington, US), was used for all studies.

### 2.2. Methods

#### 2.2.1. NanoGLA preparation

DELOS-susp methodology was used for the nanoGLA preparation ([Fig. 1](#)). An EtOH:DMSO solution (volume ratio EtOH:DMSO 4:1) containing DPPC (from 0.86 to 3.46 mg/mL), cholesterol (from 0.30 to 1.24 mg/mL), Chol-PEG<sub>400</sub>-RGD (from 0.03 to 0.31 mg/mL), and MKC (from 0.02 to 0.07 mg/mL) at a working temperature (Tw) of 308 K was loaded into a 50 mL high pressure vessel at atmospheric pressure. The solution was, then, volumetrically expanded with compressed CO<sub>2</sub> until a molar fraction ( $X_{CO_2}$ ) of 0.55 was achieved, reaching a working pressure (Pw) of 9 MPa. The system was kept at 308 K and 9 MPa under

stirring for approximately 15 min to achieve a complete homogenization and to attain thermal equilibration. A given volume of GLA stock solution at 0.28 mg/mL, measured by SDS-PAGE, was dissolved in ultrapure water to reach the desired enzyme concentration (7, 17 or 27 µg/mL). To form the nanoconjugates, the volumetrically expanded organic phase was depressurized over the aqueous solution containing the GLA. In this way, nanoGLA DELOS-susp batches of 290–500 mL were obtained. In this step, a flow of compressed N<sub>2</sub> was used as a plunger to push down the CO<sub>2</sub>-expanded solution from the vessel and to maintain a constant pressure of 10 MPa inside the vessel during depressurization. Average time per experiment was 60 min and the resulting dispersions of nanoconjugates were stored at 4 °C until their characterization. The process parameters that were kept constant for all experiments are listed in [Appendix B](#).

#### 2.2.2. Separation of the free GLA from the nanoGLA liposomal dispersion by diafiltration and concentration process

The non-conjugated GLA enzyme (with a molecular weight between 90 and 110 kDa in its dimer form) was separated from the GLA-loaded liposomes obtained by DELOS-susp using a KrossFlo Research Iii Tangential Flow Filtration (TFF) System with mPES hollow fiber modules of 300 kDa cut-off, in order to determine the GLA entrapment efficiency (EE) [4]. A volume of 10 mL of liposomal sample was added to the sample container, which was connected to the column and the buffer reservoir. Six diafiltration cycles were performed with ultrapure Type I water to eliminate the free molecules and the organic solvent present in the liposomal samples.

Concentration of the intermediate nanoGLA during the optimization step was performed using the same equipment, materials, and conditions. A volume of 50 mL of diafiltrated sample was added to the sample container and submitted to a 7.5 concentration factor, evacuating ca. 87% of water.

2.2.3. Characterization of liposomes

2.2.3.1. Mean particle size, PDI and  $\zeta$ -potential. Liposomal mean size, polydispersity index (PDI) and  $\zeta$ -potential were determined by Dynamic Light Scattering (DLS), using a Zetasizer Nano ZS analyzer (Malvern Instruments, Malvern, UK). The measurements were performed at 20 °C with a scattering angle of 173°, immediately after liposomes' preparation, and 1 and 2 weeks after the production.

2.2.3.2. Turbiscan Stability Index. Turbiscan Stability Index (TSI) was determined by Static Multiple Light Scattering (S-MLS), using a Turbiscan Lab Expert (Formulation, Toulouse, France), at 20 °C and 2 weeks after liposomes production.

2.2.3.3. Morphology. The morphology of the systems was studied using Cryogenic Transmission Electron Microscopy (Cryo-TEM). Images were obtained with a FEI Tecnai G2 12 microscope (FEI, The Netherlands) operating at 120 kV, as described in [15]. The analysis was performed 1 week after samples production.

2.2.3.4. Uni-lamellarity. Quantitative information on the liposomes degree of lamellar structure and bilayer thickness was investigated with small-angle X-ray scattering (SAXS) on an optimized NanoSTAR SAXS instrument (Bruker AXS, Karlsruhe, Germany) equipped with a

liquid Ga metal jet X-ray source (Excillum AB, Sweden) and scatterless slits. The wavelength was  $\lambda = 1.34 \text{ \AA}$  and the measurements were performed 1 week after production. The data were analyzed by a model similar to the one described in [16,17]. The model was expressed so that the fraction of bilayers presented as single-layered vesicles,  $f_{\text{single}}$ , was a fit parameter.

2.2.3.5. Entrapment efficiency. The entrapment efficiency (EE) was determined by comparing the amount of enzyme encapsulated in the nanovesicles after removal of free enzyme by diafiltration (Loaded prototype) with the amount of initial GLA present in the DELOS-susp batch just after its production (Total prototype), see Eq. (1) (Entrapment efficiency calculation):

$$EE = \frac{\text{mass GLA}_{\text{Loaded}}}{\text{mass GLA}_{\text{Total}}} \cdot 100 \tag{1}$$

To detect and quantify the enzyme in each of these samples, SDS-PAGE was performed by using gels TGX Stain-Free™ FastCast™ acrylamide 12% (Bio-Rad, ref. 161-0185). To visualize the fluorescent bands, a ChemiDoc™ Touch Imaging System (Bio-Rad) was used. Samples and standards to be quantitatively compared were run in the same gel and processed as a set. Densitometric analysis of the bands were performed with the Image Lab™ software (version 5.2.1., Bio-Rad).

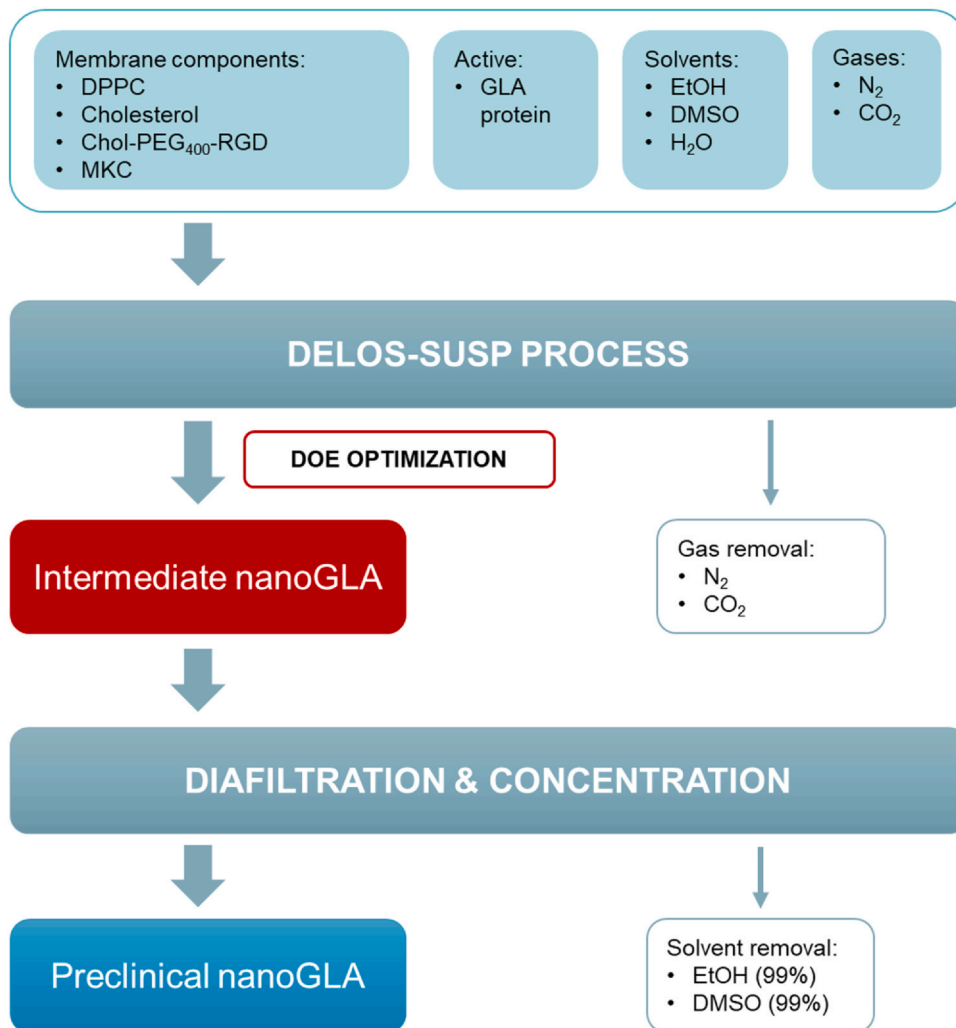


Fig. 2. Process Flow Diagram to produce the nanoGLA. Raw materials and the materials leaving the process are also represented. In red, the intermediate nanoGLA formulation obtained by DELOS-susp that has been studied in the QbD implementation. Diafiltration and concentration processes are necessary to remove the remaining free GLA and organic solvents from the nanoformulation and to maximize the enzyme concentration in the final nanoformulation for preclinical studies, respectively.

**2.2.3.6. Enzymatic activity.** The  $\alpha$ -galactosidase specific enzymatic activity (EA) of liposomal formulations was assayed using 4-Methylumbelliferyl  $\alpha$ -D-galactopyranoside (4-MUG, Sigma Chemical) as substrate, at a concentration of 2.46 mM in assay buffer (0.01 M acetic acid, pH 4.5) as previously described [18]. The released product (4-methylumbelliferone) was determined by fluorescence measurement ( $\lambda_{exc} = 365$ ,  $\lambda_{em} = 450$  nm) and final specific enzymatic activities were shown as 4-methylumbelliferone  $\mu$ mol per time and protein quantity. Measurements were performed 1 week after production of the samples.

#### 2.2.4. Experimental design and data processing

An experimental design with 4 factors at 2 levels with 2 central points (resulting in a total of 10 experimental runs) was constructed in order to study the influence of formulation parameters (independent variables or factors) on the properties (dependent variables or responses) of nanoGLA dispersion. The selected experimental design was a Fractional Factorial design, and it was developed using Modde 12 Pro software (Umetrics, Sweden). Data fitting and calculation of statistical parameters were performed by partial least squares (PLS) method. The experimental design used in this study allowed fitting the data with a linear regression interaction model. The acceptance of the responses obtained was evaluated by means of the statistical parameters predicted by the software  $R^2$ ,  $Q^2$  model validity, and model reproducibility. The design space for nanoGLA was determined using Design Space Explorer option from the Optimizer module of Modde 12 Pro software.

### 3. Results and discussion

The process flow diagram of the whole nanoGLA optimized manufacturing process is presented in Fig. 2. Membrane components, solvents, and gases, as well as the GLA protein, were processed using DELOS-susp (see Section 2) obtaining an intermediate nanoGLA dispersion, whose quality was studied by QbD. Then, the optimized intermediate nanoGLA was diafiltrated and concentrated by TFF in order to remove the organic solvents and to reach the target enzyme

concentration, which cannot be directly achieved in the DELOS-susp step because of the limited solubility of the liposome membrane components in the organic phase, while keeping the nanoformulation quality.

#### 3.1. Identification of the Critical Quality Attributes (CQAs)

During the development of liposomal drug products, the identification and pertinent characterization of CQAs of liposomal drug products is one of the main challenges from the quality point of view, together with the definition of proper control strategies. Liposomal products are complex formulations and small changes in their physicochemical attributes can have notable effects in their in vivo performance. Thus, a suitable definition of CQAs and control strategies may allow a faster and more efficient drug product development [19]. Table 1 shows the CQAs selected for QbD implementation related to the intermediate nanoGLA liposomal dispersion. The definition of the quality attributes has considered the ICH recommendations, as well as FDA and EMA guidelines [10].

As a parenteral dosage form, liposomal products must be sterile and pyrogen-free. These parameters are not considered as CQAs at this stage of formulation development since it is an intermediate product, but they must be considered as CQAs in the final formulation.

#### 3.2. Risk assessment and control strategies

Risk assessment is a valuable science-based process used in quality risk management that can aid in identifying which material attributes and process parameters potentially influence product CQAs [11,22]. The potential risk factors which might influence the quality of the product were identified through risk analysis, creating the Ishikawa diagram for each CQA defined for nanoGLA (see Appendix C, where the detailed risk analysis assessment is presented). As a result, 4 formulation factors were considered relevant to be included in the subsequent DoE analysis: GLA concentration, lipid concentration, peptide content in the liposomal membrane, and ethanol concentration. The justification regarding the

**Table 1**

CQAs defined for the intermediate nanoGLA liposomal dispersion obtained by DELOS-susp and their justification.

Quality Attribute	Justification [19–21]
Macroscopic Appearance	It must be a homogeneous opalescent dispersion without sedimentation. Sedimentation could indicate poor colloidal stability.
Mean Particle Size	Particle size and particle size distribution are major CQAs for nanoparticle-based systems, playing an important role in determining their in vivo absorption and distribution, drug loading, drug release, and targeting ability. Therefore, robust control of particle size is one of the crucial parameters for further in vivo application of liposomal drug products. Values below 300 nm are considered acceptable for nanoGLA.
Polydispersity Index (PDI)	PDI reflects the heterogeneity of the particle size, indicating how wide is the particle size distribution. The lower the PDI, the higher the homogeneity of the dispersion. To meet specification, PDI should be below 0.45.
$\zeta$ -potential	Important parameter in the evaluation of colloidal system's stability. Particles with a high negative or positive $\zeta$ -potential value repel each other, indicating that the colloidal system is stable. On the contrary, decreasing the $\zeta$ -potential value to nearly neutral could lead to liposomal aggregation. The liposome surface charge can also influence drug loading, cellular uptake, tissue distribution, and clearance. $\zeta$ -potential values higher than + 30 mV are considered inside the specification range for nanoGLA.
Particle morphology and lamellarity	Vesicles must be spheroidal and, mostly, uni-lamellar. Lamellarity can affect drug loading and release, thus, impacting the enzyme delivery.
GLA Entrapment Efficiency (EE) /Free drug substance	Free drug substance may have side effects and impact into pharmacokinetic profile. Besides, a high and reproducible percentage of drug entrapment could reduce manufacturing costs and increase drug concentration in the final formulation allowing greater flexibility in dosing. Depending on the pharmacokinetics, higher drug concentration can result in increased dosing intervals and hence improved patient compliance.
Specific Enzymatic Activity (EA)	The bioactivity of the integrated enzyme must be preserved in the nanoformulation. EA ratio to control should be higher than 0.8, referred to the EA of a commercially available GLA (agalsidase alfa, Replagal®).
Integration efficiency of Chol-PEG <sub>400</sub> -RGD in the vesicular membrane	The amount of targeting peptide moiety integrated in the nanoliposomal membrane must be in the proper ranges to allow the nanoGLA to interact with cells and facilitate intracellular penetration.
pH	pH can affect dispersion stability, drug loading and release, and cell uptake among others. A suitable pH range is from 6.0 to 7.0.
Dispersion stability	The intermediate formulation must be stable at least until the diafiltration and concentration step. In terms of Turbiscan stability, the TSI should be less than 10.0 at 24 h.
Lipid and GLA degradation products	Chemical stability of the lipid components in the liposome as well as the chemical stability of the contained drug substance is important. These will be considered at further stages of development.

selection of these factors and their range of investigation is detailed in [Table 2](#).

Although the depressurization flow rate during the DELOS-susp could be considered as a factor [30], it was not included in the present work since an accurate flow rate range variation could not be carried out in the used set-up. Due to limitations of the available in-house synthesized starting materials (GLA and Chol-PEG<sub>400</sub>-RGD), an intermediate laboratory plant was selected for performing the DoE. Thus, for this first QbD study the depressurization flow rate was kept constant at  $6.3 \pm 0.7$  g/min because it can be controlled within narrow values where the formulation requirements are ensured. So, despite not being able to introduce the flow rate as a factor in the present study, this parameter was defined as a controlled variable that was kept constant for all experiments. QbD is based on the principle of continuous improvement, thus, by gathering knowledge during early development, it is possible to avoid potential manufacturing problems as the drug product evolves through the development pipeline. Thus, the knowledge obtained in the present study will allow to concisely define further scale-up studies. The influence of DELOS-susp depressurization flow rate variation on the nanoGLA quality will be more accurately evaluated in future studies at pilot plant scale, where it is possible to control and register this parameter. Taking the present results as the basis for refining the Design Space of the nanoGLA will ease this transition from the lab to the pilot plant.

### 3.3. Experimental design and development

An experimental design was constructed to study the influence of the formulation (independent variables or factors) on the physico-chemical properties (dependent variables or responses) of intermediate nanoGLA obtained by DELOS-susp, as shown in [Table 3](#). Low and high levels for each factor ([Table 2](#)) were selected based on previous experiments and studies [4,7].

All process parameters, including depressurization flowrate at 10 g/min, were kept constant for all experiments. The responses of the experimental design were the CQAs of the intermediate nanoGLA dispersion: particle mean size, polydispersity index,  $\zeta$ -potential, Turbiscan stability index, ratio of monolayered liposomes, entrapment efficiency, enzymatic activity, and pH. Furthermore, macro and microscopic appearance (i.e. particle morphology) were analyzed, but these two CQAs were not included in the design because of their qualitative nature. The matrix of the experimental design is presented in [Table 3](#).

All experiments were produced following DELOS-susp method at the laboratory scale, as explained in [Section 2](#). All 10 experiments were produced in 2 consecutive days.

**Table 2**

Factors included in the DoE to optimize the intermediate nanoGLA formulation, their potential impact into CQAs and the ranges of investigation.

Factor	Potential impact into CQAs	Factor Range studied in DoE
GLA concentration	Protein concentration plays a key role on dispersion stability. It has been reported that increasing the loading and charge of protein will impact on size distribution and aggregation rate of the liposomal system [23].	From 7 to 27 $\mu\text{g}/\text{mL}$ of enzyme. Defined according to the viability of performing the subsequent diafiltration and concentration step up to the 200 $\mu\text{g}/\text{mL}$ required for in vivo doses.
Lipid concentration	Besides the molar ratio between membrane components (cholesterol and phospholipid), the total lipid concentration in liposomal systems will impact on its mean size, particle distribution and stability, as well as on its loading capacity [24–27].	From 1.2 to 5.0 mg/mL, moving almost 2 mg/mL up and down of previously tested concentrations in similar nanoformulations (3.0 mg/mL).
Chol-PEG <sub>400</sub> -RGD molar ratio	PEGylation of liposomes improves not only the stability and circulation time, but also the passive targeting ability on tumoral tissues, through a process known as the enhanced permeation retention effect, able to improve the therapeutic effects and reduce the toxicity of encapsulated drug [28].	From 1% to 3% mol of molar ratio in relation to the total amount of lipid components, according to previous studies.
EtOH concentration	Solvent concentration could have a direct impact on shape, solubility and electrostatic interactions between the liposomal bilayer and the loaded protein [29].	From 5% to 10% v/v, folding the standard 5% v/v since higher quantities are not recommended for intravenous administration [4].

### 3.4. Characterization of the intermediate nanoGLA obtained

A high variability on the stability of the samples was observed among the different experimental conditions tested. Thus, some characterizations were performed at the production day ( $t = 0$ ) and followed until 14 days.

Regarding the macroscopic appearance, all DELOS-susp batches presented a homogenous, whitish, opalescent appearance without presence of sediment, except for DOE-001, DOE-006, and DOE-009.

A summary of the microscopy analysis of the nanoGLA samples by cryo-TEM is presented in [Fig. 3](#), indicating that for all experiments nanovesicles were obtained, being mostly uni-lamellar and spherical, and ranging between 100 and 200 nm, with the presence of some larger vesicles around 500 nm.

[Table 4](#) shows a summary of the characterization results of the DoE samples, which were considered for the statistical analysis. The three out of ten batches (DOE-001, DOE-006, and DOE-009) that presented small sedimentation also showed a higher TSI indicating the dispersion instability.

Besides, samples in which aggregation and sedimentation were observed presented also higher size and PDI, and lower uni-lamellarity. Furthermore, the mean particle size and PDI of DOE-001, DOE-006, and DOE-009 significantly increased with time after production ([Appendix D](#)). On the other side,  $\zeta$ -potential, EE, and EA values did not correlate with macro and microscopical characteristics of the samples.

All the formulations showed enzymatic activity, varying from 0.8 to 1.7 ratio to control referred to the enzymatic activity of a commercially available free GLA (Agalsidase alfa, Replagal® from Shire-Takeda) included in the analysis, as also shown in [Table 4](#). These results indicate an excellent enzymatic activity in all cases, compliant with preliminary specifications.

### 3.5. Analysis of the influence of the factors on CQAs

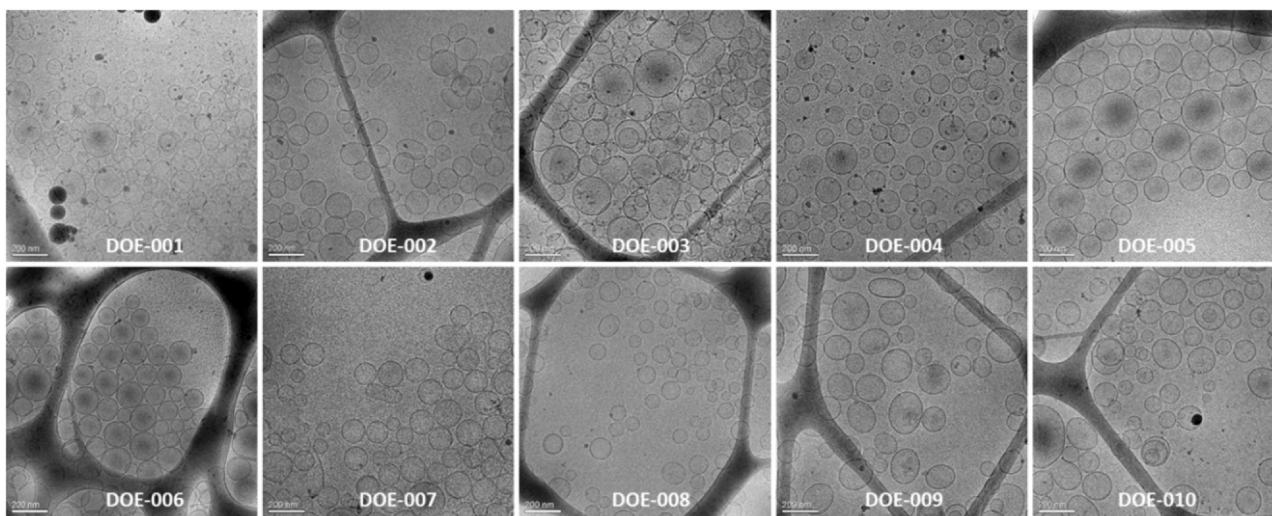
The influence of the factors was studied for the rest of dependent variables or CQAs. An analysis and discussion for each quantifiable CQA is described below. From the characterized CQAs, mean particle size,  $\zeta$ -potential, and uni-lamellarity could be statistically fitted and were included in the prediction model (see [Appendix E](#) for modeling and data fitting) while for the rest of attributes a bad correlation was obtained and thus a poor predictive ability of the model.

According to the data presented in [Table 4](#), the mean particle size of the nanoGLA dispersions varied from 90 to 200 nm. These differences could be explained because of the aggregation and fusion of liposomal vesicles that could occur 1 week after preparation. The coefficients of the equation describing the influence of the factors on nanoGLA particle

**Table 3**

Matrix of experimental design. The sample codes consider the randomized order of experiments.

Experimental run	GLA concentration ( $\mu\text{g/mL}$ )	Lipid concentration ( $\text{mg/mL}$ )	Chol-PEG <sub>400</sub> -RGD molar ratio to lipids (% mol)	EtOH concentration (% v/v)
DOE-001	27	1.2	1	10.0
DOE-002	7	1.2	3	10.0
DOE-003	17	3.1	2	7.5
DOE-004	27	5.0	1	5.0
DOE-005	7	5.0	3	5.0
DOE-006	27	1.2	3	5.0
DOE-007	17	3.1	2	7.5
DOE-008	7	1.2	1	5.0
DOE-009	27	5.0	3	10.0
DOE-010	7	5.0	1	10.0

**Fig. 3.** Representative cryo-TEM images of nanoGLA DoE samples at 1 week after production. Scale bar 200 nm.**Table 4**Characterization of intermediate nanoGLA CQAs after 1 week of production. Uncertainties are calculated from the standard deviation of measurement for Size, PDI,  $\zeta$ -potential, and EE; and from standard error of the mean for uni-lamellarity and EA.

Sample ID	Size (nm)	PDI	$\zeta$ -potential (mV)	TSI	Uni-lamellarity, $f_{\text{single}}$	EE (%)	EA (ratio to control)
DOE-001 <sup>a</sup>	143 $\pm$ 6	0.45 $\pm$ 0.08	35 $\pm$ 2	11.5	0.88 $\pm$ 0.01	60 $\pm$ 1	1.7 $\pm$ 0.1
DOE-002	88 $\pm$ 2	0.17 $\pm$ 0.01	36 $\pm$ 2	0.6	0.99 $\pm$ 0.01	53 $\pm$ 1	1.2 $\pm$ 0.0
DOE-003	142 $\pm$ 3	0.12 $\pm$ 0.05	34 $\pm$ 0	1.2	0.95 $\pm$ 0.00	59 $\pm$ 1	1.4 $\pm$ 0.0
DOE-004	175 $\pm$ 1	0.32 $\pm$ 0.05	45 $\pm$ 0	8.2	0.93 $\pm$ 0.00	45 $\pm$ 1	1.6 $\pm$ 0.1
DOE-005	158 $\pm$ 4	0.24 $\pm$ 0.03	45 $\pm$ 6	1.9	0.93 $\pm$ 0.00	42 $\pm$ 1	0.8 $\pm$ 0.1
DOE-006 <sup>a</sup>	202 $\pm$ 4	0.46 $\pm$ 0.05	32 $\pm$ 1	6.6	0.85 $\pm$ 0.02	68 $\pm$ 1	1.5 $\pm$ 0.0
DOE-007	146 $\pm$ 2	0.11 $\pm$ 0.05	35 $\pm$ 1	1.2	0.99 $\pm$ 0.01	53 $\pm$ 1	1.2 $\pm$ 0.2
DOE-008	100 $\pm$ 1	0.17 $\pm$ 0.02	38 $\pm$ 1	1.8	1.00 $\pm$ 0.01	84 $\pm$ 1	0.8 $\pm$ 0.0
DOE-009 <sup>a</sup>	172 $\pm$ 5	0.22 $\pm$ 0.02	38 $\pm$ 1	12.0	0.94 $\pm$ 0.01	53 $\pm$ 1	1.1 $\pm$ 0.1
DOE-010	134 $\pm$ 2	0.13 $\pm$ 0.02	46 $\pm$ 2	0.6	0.93 $\pm$ 0.00	84 $\pm$ 1	1.4 $\pm$ 0.1

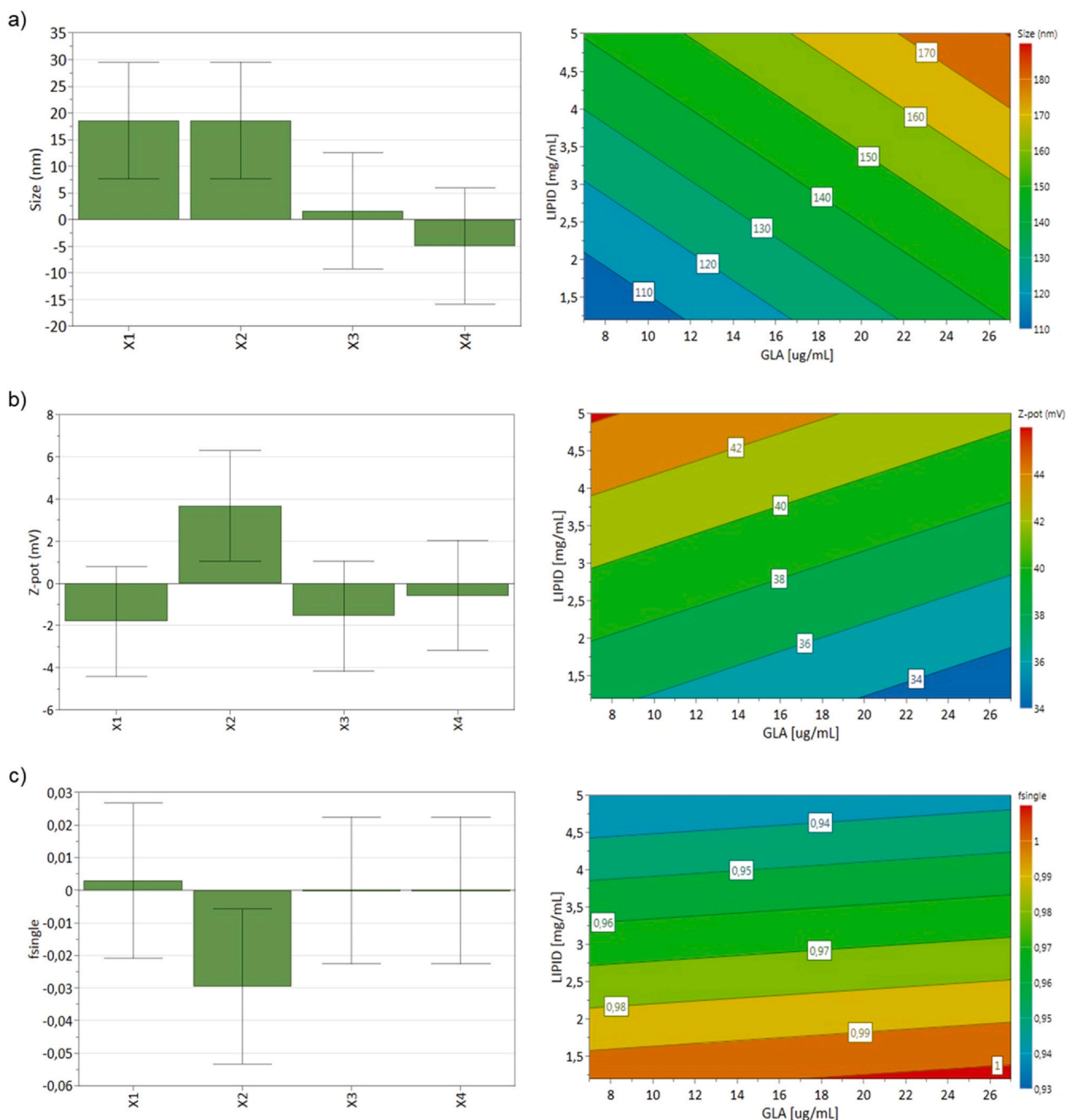
<sup>a</sup> DOE-001, DOE-006, and DoE-009 presented sedimentation.

size are shown in Fig. 4a (left). According to this figure, the size of nanoGLA liposomes is significantly influenced by GLA concentration (X1) and the lipid concentration (X2). Thus, a significant increase in size is obtained when the concentration of GLA and lipid increase. The increase in size with the increase of GLA and lipid concentrations could be explained by the occurrence of physical aggregation of the vesicles. The influence of GLA and lipid concentration is also illustrated by the contour plot for size in Fig. 4a (right).

As shown in Table 4,  $\zeta$ -potential ranged from 32 to 46 mV for non-diafiltrated liposomes. The influence of studied factors on  $\zeta$ -potential is shown as coefficients of the regression equation plot in Fig. 4b (left). According to this plot, lipid concentration (X2) was the only factor that had a significant positive effect on the  $\zeta$ -potential of the dispersions obtained. This could be explained because when lipid concentration

increases, MKC surfactant (used as excipient in the nanoformulation) concentration also increases, giving more positive charges to the liposomal system. The influence of lipid concentration is also illustrated by the contour plot for size in Fig. 4b (right).

Monolayered liposomes fractions varied from 0.88 to 1.00, as shown in Table 4 by  $f_{\text{single}}$  values. According to Fig. 4c (left), lipid concentration was the only factor affecting this CQA significantly, showing a larger difference in comparison to the rest of factors. As can be seen in Fig. 4c (right), GLA concentration had an insignificant influence on the monolayer ratio of liposomes, but it was strongly affected by the lipid concentration. The explanation can be the same as the effect of lipid concentration on vesicle size: aggregation and fusion of the vesicles when lipid concentration increases could be responsible of this behavior.



**Fig. 4.** Left side: scaled and centered coefficients of the regression equations describing the influence of formulation parameters X1-GLA concentration, X2-lipid concentration, X3-Chol-PEG<sub>400</sub>-RGD molar ratio, X4-EtOH concentration, on the liposomes size,  $\zeta$ -potential, and uni-lamellarity of nanoGLA intermediate dispersion. Right side: contour plots for the same CQAs of the nanoGLA intermediate dispersion. Molar ratio of chol-PEG<sub>400</sub>-RGD to lipid and EtOH concentration were kept constant at 2% mol and 7.5% v/v, respectively.

### 3.6. Evaluation of the design space

Among all the factors studied, GLA concentration and lipid concentration were found to have a significant influence on some of the responses. Thus, the Design Space for intermediate nanoGLA was constructed using these factors which significantly influenced the quality of the nanoformulation. On the one hand, increase of GLA and lipid concentration had a negative influence on liposomal mean particle size because of the size increase promoted by aggregation. On the other hand, as the lipid concentration increased, and consequently, the amount of MKC surfactant was higher,  $\zeta$ -potential (which is related to the electrical charge at the liposomes surface) also increased due to the formal positive

charge provided by this cationic surfactant. Nevertheless, this  $\zeta$ -potential increase was not correlated with a higher colloidal stability of the nanoformulation as also confirmed by an uni-lamellarity decrease. It seems that this MKC amount is not enough to stabilize such highly concentrated samples. However, higher MKC concentrations, although could improve the stability of these concentrated samples, it also could entail a toxicological concern as well as the abolishment of the enzymatic activity of the GLA, as reported by Tomsen-Melero et al. [7].

The other CQAs such as polydispersity index, TSI, GLA entrapment efficiency, and enzymatic activity could not be fitted in any reliable model because of the sedimentation of some batches and the high characterization variability, due to the use of SDS-PAGE plus TGX as a reference method for



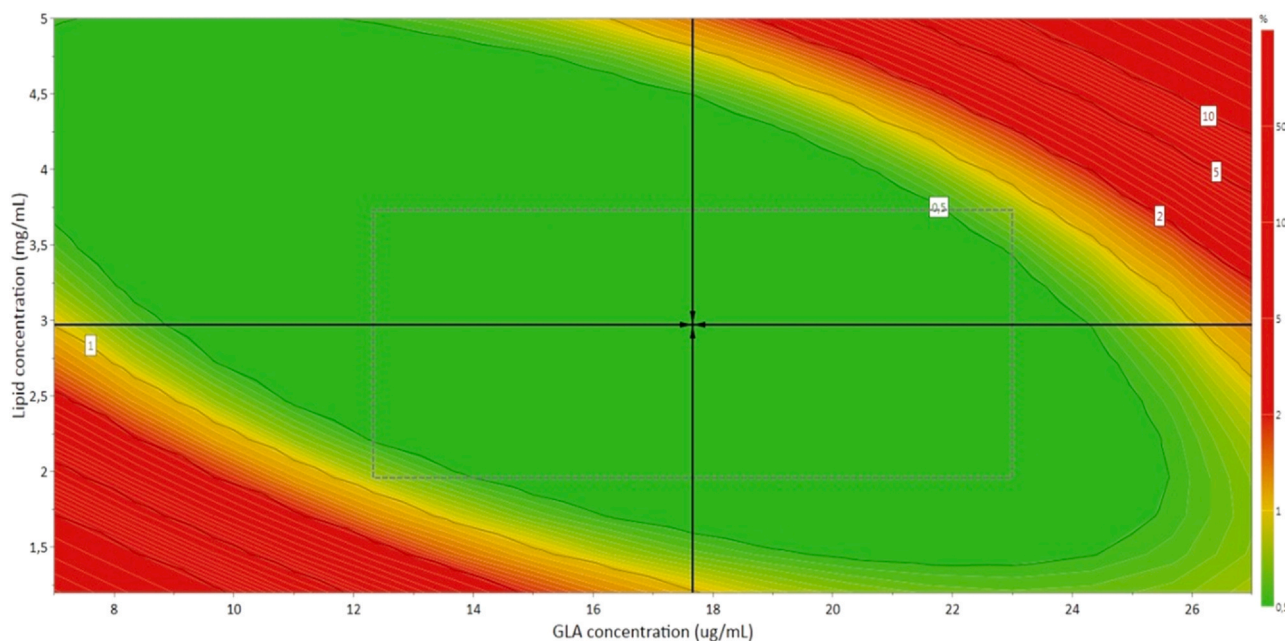


Fig. 5. The Design Space for intermediate nanoGLA liposomal dispersion that meets the specifications in terms of CQAs, expressed as the probability of failure (%). Molar ratio of chol-PEG<sub>400</sub>-RGD to lipid and EtOH concentration have been optimized in the run at 1.16% mol and 6.2% v/v, respectively.

Table 5

The desired CQAs of nanoGLA introduced in the Design Space explorer and their values.

Response	Criterion	Min.	Target	Max.
Size (nm)	Target	50	150	250
ζ-potential	Excluded	–	–	–
Uni-lamellarity ( $f_{single}$ )	Maximize	0.95	1.00	–

GLA quantification. Results could be improved in the future using a HPLC method for the quantification of GLA. Hence, the Design Space was determined using particle size, ζ-potential, and uni-lamellarity.

The Design Space obtained is shown as the green region in Fig. 5, and shows the combination of factors for which the nanoGLA intermediate obtained by DELOS-susp will meet the specifications in terms of CQAs, specified in Table 5, with a probability of failure less than 1%. The combination inside the design space which is pointed out by the black arrows indicates the robust setpoint (17.7 µg/mL GLA concentration, 2.97 mg/mL lipid concentration, 1.3% mol Chol-PEG<sub>400</sub>-RGD, and 6.2% v/v EtOH) corresponding to the formulation for which the prediction errors are the lowest.

To our knowledge, there are no similar results reporting the relationship between lipid and protein concentration affecting size, ζ-potential, and uni-lamellarity in this way. We could expect that at low concentration of lipid and GLA, we would also obtain a nanoGLA within the established acceptance limits, so it could be possible that the red zone showed in Fig. 5 around the lowest concentrations belongs to a range that remained unexplored. In addition, the finding of a model which indicates that formulation will escape from the acceptance limits

Table 6

Critical Quality Attributes for optimized intermediate nanoGLA, diafiltrated and concentrated around 10-fold.

Attributes	After DELOS-susp (Intermediate nanoGLA)	After concentration (Preclinical nanoGLA)
Stability	NA	> 2 weeks
Particle mean size (nm)	138 ± 7	165 ± 3
Polydispersity Index	0.38 ± 0.03	0.41 ± 0.02
ζ-potential (mV)	40 ± 1	35 ± 1
Enzymatic activity (ratio to control)	1.11 ± 0.08	0.93 ± 0.04
GLA (µg/mL)	34 ± 2	330 ± 20

if both factor concentrations are high is due to aggregation effect of liposomes caused by a change of interaction between them, provoked by the high load of components in the membrane [24,31].

### 3.7. Optimization of the nanoGLA formulation

The challenge was to obtain a stable nanoGLA concentrated formulation containing 200 µg/mL of GLA, suitable doses for in vivo testing. To do so, a batch of nanoGLA was prepared by DELOS-susp and diafiltrated and concentrated following the trend of the preliminary Design Space: the lipid concentration was reduced to 1.2 mg/mL so that the GLA concentration could be increased up to 35 µg/mL, obtaining an intermediate nanoGLA by DELOS-susp meeting all the CQAs.

Physicochemical properties are shown in Table 6 and Fig. 6. Particle mean size, polydispersity index, ζ-potential, and GLA concentration – all meet the requirements to go to future in vivo preclinical trials (< 300 nm, ≤ 0.45, > 30 mV, and > 200 µg GLA/mL, respectively). A good colloidal stability was observed for the concentrated final nanoGLA, composed mainly by single lamellar liposomes (Fig. 6). Some structural effects were noticeable by cryo-TEM after over-concentrating the GLA-loaded liposomes. Images revealed the formation of some multilamellar complexes, where the GLA can be identified between liposomal layers as well as inside the vesicles (Fig. 6, arrows), forming structures resembling lipoplexes [32]. Interestingly, the high concentration of GLA (330 µg/mL) after the concentration process where these structures were identified was quite above the minimum required value for in vivo trials (200 µg/mL).

In addition, the final prototype dispersion was stable for more than 2 weeks.

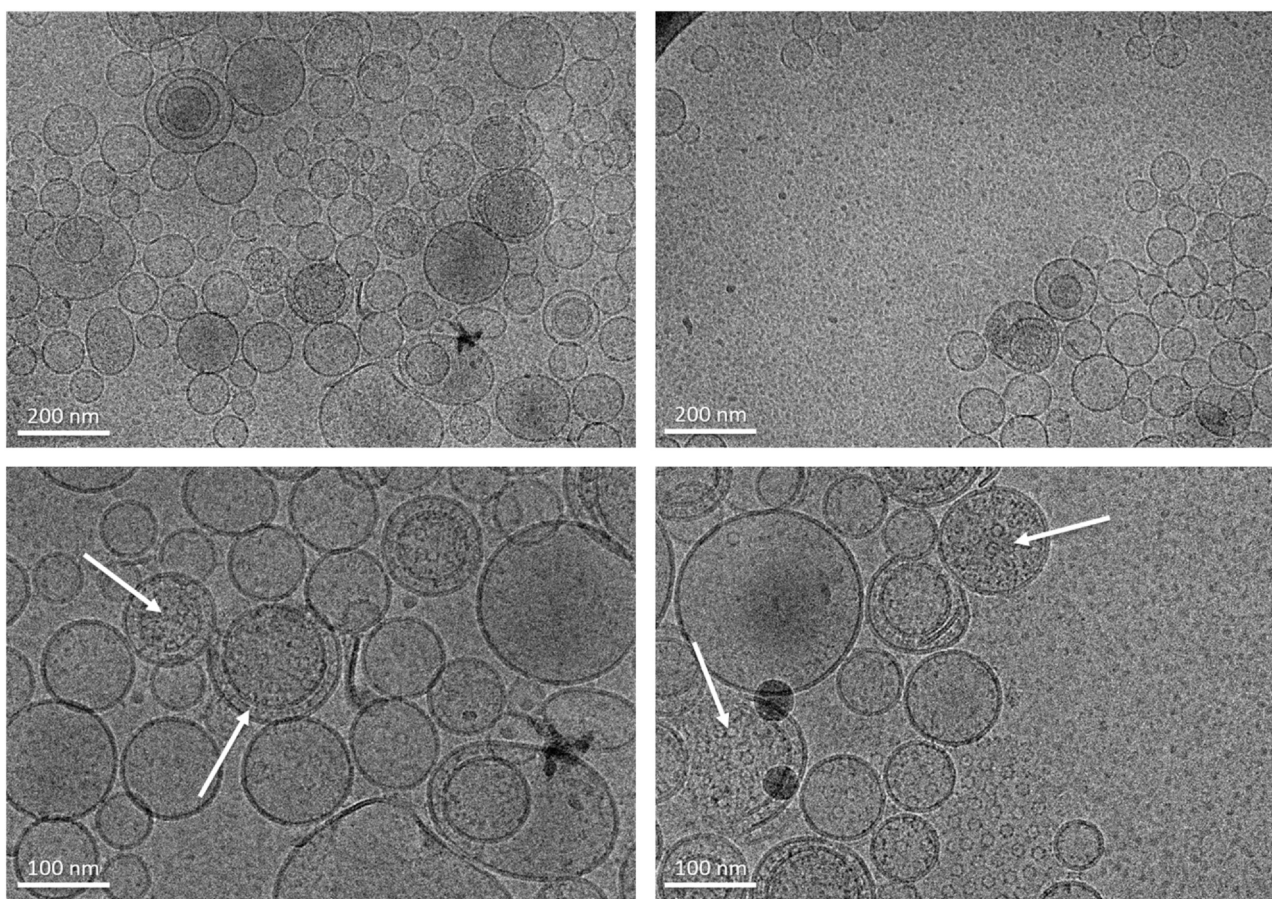


Fig. 6. Cryo-TEM images of optimized nanoGLA prototype after concentration. The images were acquired 2 weeks after production.

### 3.8. Safe-by-Design implementation

The implementation of the SbD approach followed the strategy reported by [33] and was specifically tailored to complement the QbD work, to prevent hazards from the developed components and processes, and to support the redesign of technical workflows where the need is identified. Each individual process step was evaluated to identify possible exposure scenarios and safety issues.

For the used DELOS-susp methodology (see Fig. 2), four specific issues that pose a potential risk were identified:

1. DMSO/EtOH in the nanoformulation
2. Aerosol exposition due to organic compounds, vapors, streams from the organic phase
3. Carbon dioxide poisoning
4. Cold burn during lyophilization

All the identified possible risks during the DELOS-susp methodology are rated on low respectively medium risk level and are controlled (see Appendix F), thus the DELOS-susp process can be considered as safe. To fully cover the entire innovation process towards its final product application, immunogenicity, endotoxicity, and impurities of the nano-formulation will be evaluated at later stage.

## 4. Conclusions

The current work brings a new contribution in the preparation of GLA loaded liposomes through the successful application of the QbD approach to DELOS-susp production method. Thanks to this methodology a

prototype of nanoGLA suitable for in vivo testing could be optimized. The influence of some formulation parameters was determined by using a DoE. Thus, among the formulation factors, GLA concentration and lipid concentration were the most important parameters for the quality of nanoGLA obtained by compressed fluid processing.

This study also enabled the obtaining of a preliminary design space to produce nanoGLA intermediate dispersion, in which the established quality requirements of the product are met.

Through the design space analysis, it could be predicted that for achieving a higher (10-fold), concentration of enzyme in the final formulation the concentration of lipid in the DELOS-susp step could be reduced in order to obtain a good quality product in terms of particle size and uni-lamellarity, and to avoid aggregation and sedimentation.

### Declaration of Competing Interest

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests: J.L.-C., D.P., S.Sch., M.R., I.A., J.V., S.Sa. and N.V. are inventors of patent WO/2014/001509 licensed to Biopraxis Research AIE. J.V., S.Sa. and N.V. are inventors of patent WO/2006/079889 owned by Nanomol Technologies SL, and stock-owners in Nanomol Technologies SL. J.M.-M., J.T.-M., A.F., E.G.-M., J.-L.C, E.C.-L., D.P., M.R., S.Sch., I.A., A.S., S.Sa., J.V., N.V. and A.C. are inventors of patent application EP21382062.4.

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UAB SepBioES scientific-technical service ([www.nanbiosis.es/unit/u1-proteinproduction-platform-ppp/](http://www.nanbiosis.es/unit/u1-proteinproduction-platform-ppp/)), the Soft Materials Service linked to Biomaterial Processing and Nanostructuring Unit at ICMAB-CSIC ([www.nanbiosis.es/portfolio/u6-biomaterial-processing-and-nanostructuring-unit/](http://www.nanbiosis.es/portfolio/u6-biomaterial-processing-and-nanostructuring-unit/)) and the Peptide Synthesis unit at the IQAC-CSIC ([www.nanbiosis.es/portfolio/u3-synthesis-of-peptides-unit/](http://www.nanbiosis.es/portfolio/u3-synthesis-of-peptides-unit/)).

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## Appendix A. Synthesis of GLAcmycHis

### *Plasmids and E. coli strains*

The GLA gene was obtained from the commercial vector pReceiver-M10 (OmicsLink ORF Expression Clone, ref. EX-Q0172-M10), that encodes a cDNA version of the GLA gene (primary gene accession number: [NM\\_000169](https://www.ncbi.nlm.nih.gov/nuccore/NM_000169)), in which both c-myc and 6xHis tags are fused (for further detection and purification purposes) to the C-terminus.

For further steps, the pOptiVEC™-TOPO® TA Cloning Kit (Catalog Number 12744-017, Invitrogen, by Life Technologies) was used following the vendor protocol. The PCR product was cloned into the pOptiVEC™-TOPO® plasmid, and the resulting plasmid (pOptiVec-GLA) was transformed into TOP10 *E. coli* cells. Positive clones were selected by ampicillin and confirmed by restriction analysis. The pOptiVec-GLA plasmid was purified by “gigaprep” method, and finally linearized before transfection, as recommended by the vendor, with restriction enzyme *PvuI*. All plasmids were purified from their corresponding overnight bacterial cultures, using the EndoFree Plasmid Giga Kit (Qiagen, ref. 12391). For their quantification, absorbances at 260 nm (A260) and 280 nm (A280) were measured.

### *Mammalian cell line, transfection and selection of positive clones*

For the transfection and further selection of CHO cells overexpressing the human GLA enzyme, the OptiCHO™ Express Kit (Catalog number 12745-014, Invitrogen, by Life Technologies) was used. This kit provides CHO DG44 cells, media and transfection reagent needed. DG44 dhfr- CHO cells were grown in CD DG44 medium with 8 mM L-glutamine, at 37 °C in 8% CO<sub>2</sub> using standard techniques.

Transfection of CHO DG44 cells and selection of positive GLA-DHFR cells were performed following the vendor protocol. At 28 days post-transfection, stepwise selection for dhfr amplification was started, using two-fold increments of methotrexate hydrate (MTX, Sigma, catalog number A6770) starting at 50 nM up to 4 μM. Finally, and in order to obtain a single clone, the pool of stably transfected and 4 μM MTX-amplified cells were serially diluted and seeded at 1–2 cells per well in a 96-well plate. As suggested by vendor, to grow CHO DG44 cells under adherent conditions, the specific medium Gibco® CD-CHO-A was used. After this process, a single clone (namely CHO-DG44-GLA clone #3) was isolated and cryopreserved.

### *Cryopreservation of CHO-DG44-GLA clone #3*

CHO-DG44-GLA clone #3 was cultured in complete CD OptiCHO medium (supplemented with L-Glutamine 8 mM) to  $2 \times 10^6$  cells per milliliter and then centrifuged at 100 g for 5 min. Cell pellets were then resuspended in fresh medium containing 10% DMSO to a final cell concentration of  $10 \times 10^6$  cells/mL. Cells were aliquoted into 1 mL cryovials (Nalgene) and stored in the vapor phase of liquid nitrogen.

### *Production and purification of extracellular GLAcmycHis protein*

Cryovials of CHO-DG44-GLA clone #3 were thawed under standard procedures. Briefly, cryovial was rapidly thawed at 37 °C and resuspended in 15 mL of prewarmed complete CD OptiCHO medium. Cells were expanded by subculturing them up to the desired volume. In each passage, cells were diluted into pre-warmed complete CD DG44 Medium to give a final cell density of  $2 \times 10^5$ – $3 \times 10^5$  viable cells/mL. Finally, supernatant containing extracellular GLAcmycHis was harvested by centrifuging the cell culture at 14,000 rpm for 15 min. This supernatant was purified in an ÄKTA Pure system (GE Healthcare) by using an affinity chromatography column (HisTrap Excel 5 mL, Ref 17-3712-06, GE Healthcare) following the vendor protocol. Finally, the eluted protein was dialyzed in acetic buffer 0.01 M pH 5.5 and stored at –20 °C until used.

Appendix B. DELOS-susp methodology for the preparation of nanoGLA

Table B.1 summarizes the process parameters that were kept constant for all DELOS-susp experiments; and also includes the control strategies since some of them could have an impact on some CQAs. The 10 experiments carried out in this study were produced in 2 consecutive days.

Table B.1  
DELOS process parameters kept constant in all DoE experimental runs.

Process Parameter	Value	Control
Working temperature, Tw	35 °C	Heating jacket
High pressure stirring	500 rpm	Magnetic stirrer controller
Working pressure, Pw	9 MPa	Syringe pump for CO <sub>2</sub>
Depressurization pressure in the autoclave	10 MPa	Manometer and N <sub>2</sub> pressure regulator
Collector Stirring	300 rpm	Plate with magnetic stirrer
CO <sub>2</sub> molar fraction, X <sub>CO2</sub>	0.55	Solvent volume in the reactor
Depressurization flowrate	10 g/min	Manually controlled due to scale, averaged
Collector temperature	23 °C	Monitored, room temperature

Appendix C. Risk analysis assessment

Fig C.1 represents a summary of Critical Material Attributes (CMAs) and Critical Process Parameters (CPPs) that may impact the CQAs of the intermediate nanoGLA using Ishikawa methodology.

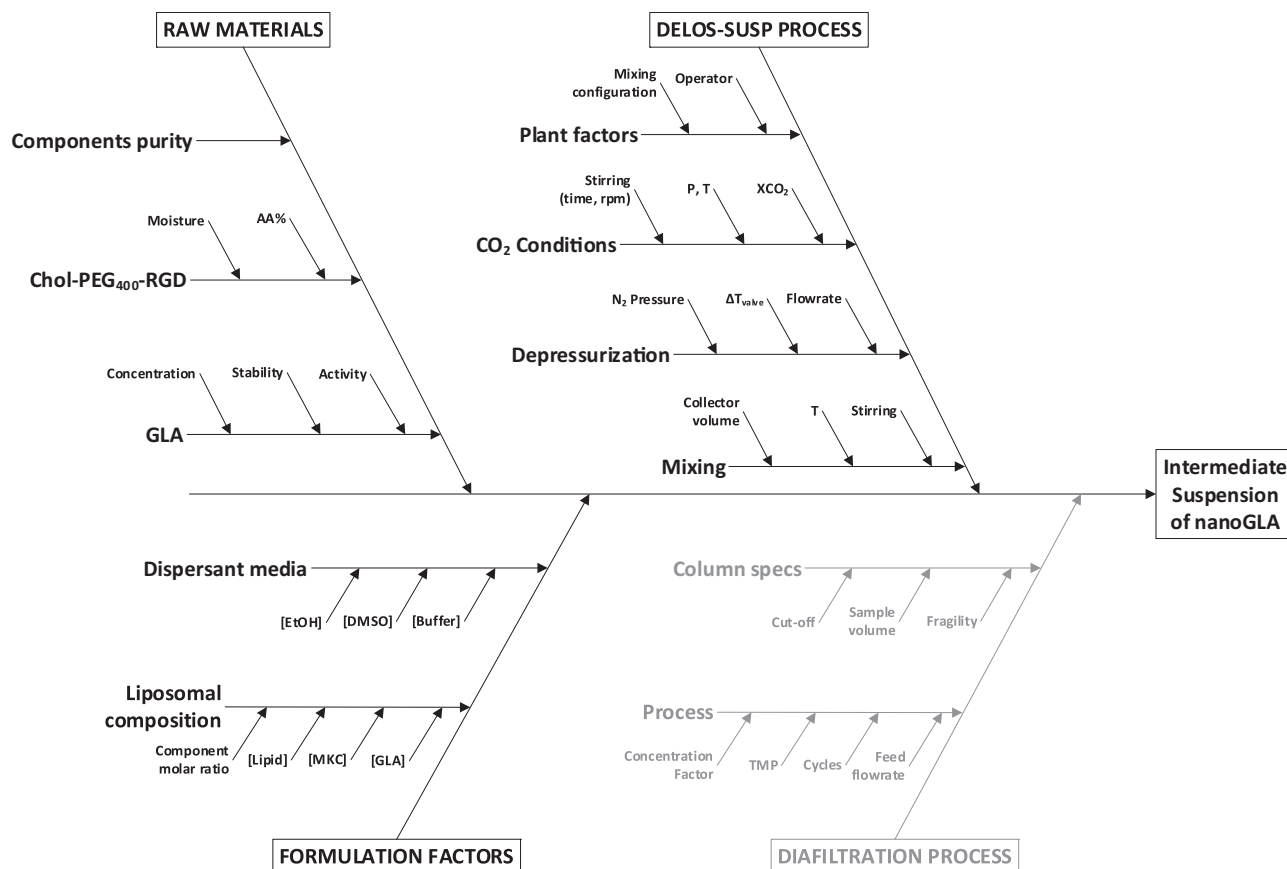


Fig. C.1. Ishikawa diagram illustrating the summary of CPPs and CMAs that may impact on each selected CQA of intermediate nanoGLA dispersion.

A control strategy is designed to ensure that a product of required quality will be produced consistently. These controls are based on product, formulation and process understanding and should include, at a minimum, control of the critical process parameters and material attributes. The risk assessment and the definition of control strategies serve to evaluate which CMAs and CPPs must be studied in a DoE.

In Table C.1 the risk analysis assessment of the potential CMAs and CPPs on the DELOS-susp process is presented.

**Table C.1**

Risk analysis assessment and control strategies of CMAs and CPPs for intermediate nanoGLA production by DELOS-susp.

CMA or CPP	Impact on CQA	Risk	Control strategy
Components purity	Low	Change in composition	CoA from supplier
Raw GLA	High	Change in morphology, nanoGLA stability an activity	CoA from supplier and check analysis by TGX, BCA or HPLC.
Chol-PEG <sub>400</sub> -RGD AA%	Low	Affect biological activity	CoA from supplier and check analysis
Chol-PEG <sub>400</sub> -RGD moisture	Low	Uni-lamellarity and morphology could be affected.	CoA from supplier and check analysis
EtOH concentration	High	To be evaluated in DoE.	To be included in DoE.
DMSO concentration	Medium	Stability, enzymatic activity	Previously defined.
Buffer concentration	Medium	To be studied in further steps.	To be defined in further steps of the project.
Membrane components molar ratio	High	Morphology, stability	Previously defined.
Lipid concentration	High	Entrapment efficiency, stability of the solution.	To be included in DoE.
Chol-PEG <sub>400</sub> -RGD concentration	High	Morphology, stability, intracellular penetration	To be included in DoE.
MKC concentration	High	Higher concentration, higher stability and Entrapment.	Previously defined.
GLA concentration	High	Stability, enzymatic activity	To be included in DoE.
Mixing configuration	High	Morphology, stability	Previously defined.
Operator	Low	Low control of the flowrate	Lab scale: Follow the standard protocol and practice on depressurization. Pilot scale: automatic control of depressurization valve.
Stirring of vessel	Low	Enough to obtain a single phase inside the high pressure vessel.	Previously defined, servocontrolled by high pressure stirrer.
Pressure of vessel	Low	Enough to obtain a liquid phase inside the high pressure vessel.	Previously defined, servocontrolled by pump and PIC.
Temperature of vessel	Low	Enough to obtain a liquid phase inside the high pressure vessel.	Previously defined, controlled by heating jacket and TIC.
CO <sub>2</sub> molar fraction	Low	Inside the range of cosolvency.	Previously Defined and controlled by volume, P and T of the pump.
N <sub>2</sub> pressure	Low	10 bar higher than pressure of the vessel, could affect the flowrate.	Defined and controlled by a pressure regulator and PIC
Flowrate	High	Morphology and uni-lamellarity. To be evaluated in DoE.	To be included in DoE.
Collector volume	Medium	Change in flow and mixing between phases.	Previously defined.
Collector temperature	High	GLA degradation depends on temperature and exposition time	Previously defined. Controlled by TIC.
Stirring of the collector	Medium	Change in flow and mixing between phases.	Previously defined.

#### Appendix D. Samples time evolution of mean particle size, PdI, and $\zeta$ -potential

Fig D.1 shows the analysis in time by DLS of the samples. As the Fig D.1. Evolution shows, the mean size of some samples increased during time, mainly explained by the aggregation of the nanovesicles, showing clearly that DOE-006 and DOE-009 were going to sediment. PdI values, remained constant except for the two samples previously mentioned.  $\zeta$ -potential maintained mostly constant with time, although the decrease observed in some cases could be explained because of the change in pH during time caused by the release of dissolved CO<sub>2</sub>.

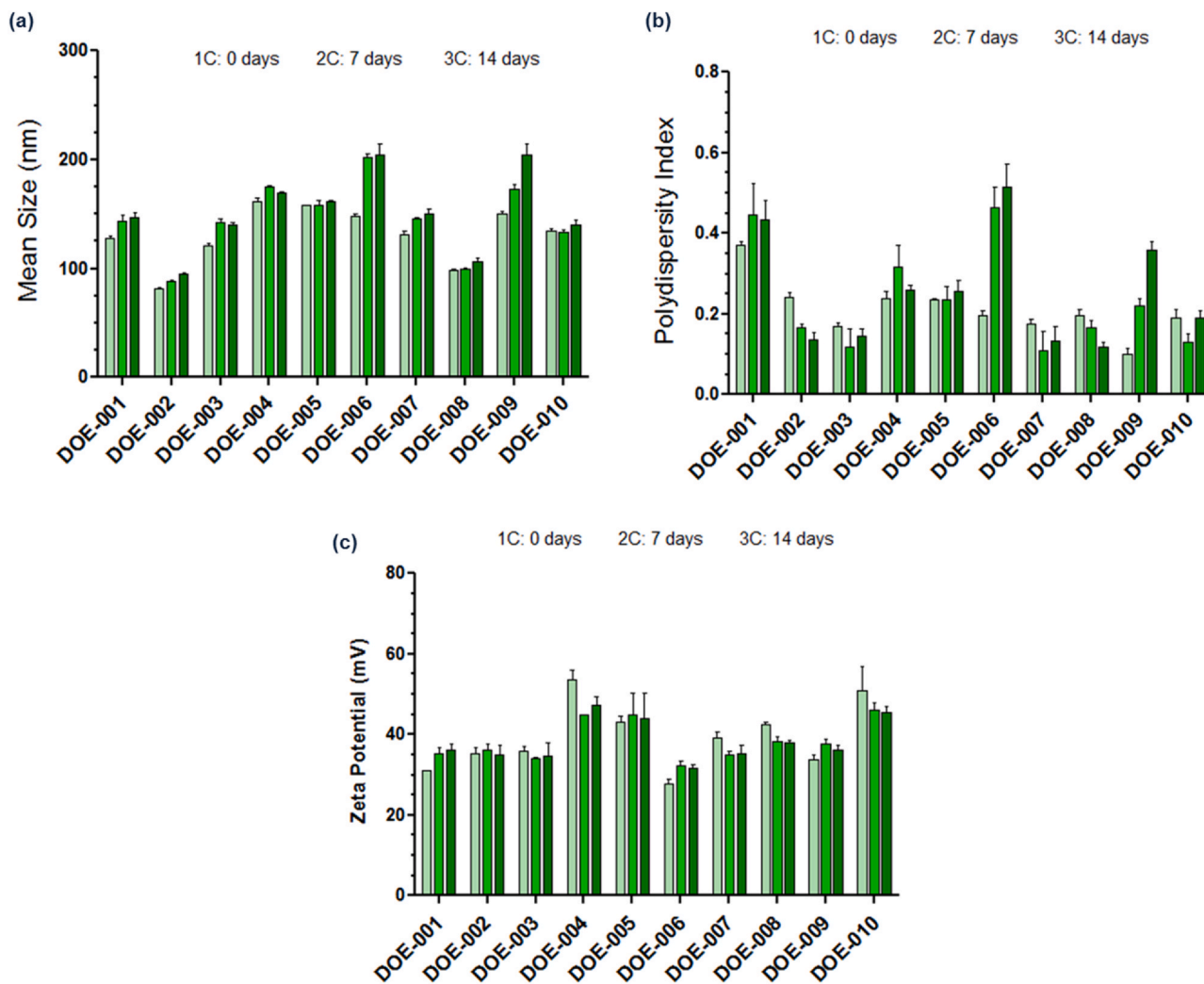


Fig. D.1. Evolution of a) mean particle size, b) PDI, and c)  $\zeta$ -potential over time during 14 days after the production of the samples.

### Appendix E. Modeling and data fitting

The acceptance of the responses obtained was evaluated by means of the statistical parameters predicted by the software  $R^2$ ,  $Q^2$  model validity, and model reproducibility: (i)  $R^2$ : it represents the percent of the variation of the response explained by the model, that is, how well the model fits the data; (ii)  $Q^2$ : it is the percent of the variation of the response predicted by the model according to cross validation. It gives information about how well the model predicts new data. In Table E.1, the values of these statistical parameters are summarized, indicating if the data collected from the experimental results is fitting into a model. Only those CQAs that could be fitted (mean particle size,  $\zeta$ -potential and uni-lamellarity) were included in the model.

**Table E.1**  
Statistical parameters and fitting for the investigated intermediate nanoGLA CQAs.

CQA	$R^2$	$Q^2$	Fitting and model (if applies)
Mean particle size	0.937	0.661	Yes, Size = $2.0 X_1 + 10.6 X_2 + 11.7 X_3 - 2.2 X_4 + 86$
Polydispersity	0.437	0.200	No, a bad correlation and a poor predictive ability of the model were obtained.
$\zeta$ -potential	0.791	0.550	Yes, $\zeta\text{-pot} = -19 X_1 + 2.1 X_2 - 10.9 X_3 - 24.5 X_4 + 41$
TSI	0.636	0.200	No, a bad correlation and a poor predictive ability of the model were obtained.
Uni-lamellarity	0.858	0.498	Yes, $f_{\text{single}} = 3.3 \cdot 10^{-4} X_1 - 1.8 \cdot 10^{-2} X_2 - 1.1 \cdot 10^{-7} X_3 - 5.7 \cdot 10^{-9} X_4 + 1.0$
Entrapment efficiency	0.420	0.200	No, a bad correlation and a poor predictive ability of the model were obtained.
Enzymatic activity	0.625	0.040	No, it could be explained by the high measurement related variability

### Appendix F. Identified safety issues

Occupational exposure scenarios as well as environmental exposure scenarios were registered, considering different operational conditions. Table F.1 shows the obtained risk rating key for the specific activity and/or process in the DELOS-susp methodology for the preparation of the nanoGLA intermediate, and lists relevant methods to manage the possible risk and decrease its possibility to take place.

Table F.1

Identified safety issues in relation to their severity and likelihood leads to risk rating key.

Activity/Process	Associated Risk(s): Safety issue(s) associated with the activity	Severity: Level of impact	Likelihood: The chances of that risk happening	Method(s) to Manage the Risk: A list of methods you will use to minimize the chances of the risk happening
<b>Preparation of the organic solution</b>	EtOH/DMSO in the nanoformulation	Acceptable	Low	Related to the environment: Solvents to the non-chlorinated solvents waste container. Cholesterol, Chol-PEG <sub>n</sub> -RGD, MKC, and DPPC to the solid chemical waste container.
<b>Weighing solids and preparation of a solution</b>	Dermal/occupational safety issues during cleaning	Acceptable	Low	Related to workers: Fume hood. Mask, gloves, glasses and lab coat.
<b>Cleaning the laboratory material</b>				
<b>Loading of the vessel, closing and pressurization by adding CO<sub>2</sub></b>	Dermal/occupational safety issues during loading the vessel	Acceptable	Low	Related to workers: Fume hood. Mask, gloves, glasses, and lab coat. Vent and safety valves present in the equipment in case of overpressure
<b>Preparation of aqueous solution</b>	Dermal safety issues during cleaning of the material	Acceptable	Low	Related to workers: Fume hood. Mask, gloves, glasses, and lab coat.
<b>Depressurization and mixing of the organic and aqueous phases</b>	Carbon dioxide poisoning during valve opening	Tolerable	Low	Related to workers: Fume hood. Mask, gloves, glasses and lab coat. Vent and safety valves. Filters for carbon dioxide exhaust expelled to the environment have to be considered in larger scales.
<b>Collecting the final product and storage</b>	Cold Burn during lyophilization	Acceptable	Low	Fume hood. Mask, gloves, glasses and lab coat.

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