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1 **Dielectric Heating: A Review of Liquid Foods Processing Applications**

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12
13 **Short title**

14 **Dielectric Heating of Liquid Foods**

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23 **Dielectric Heating: A Review of Liquid Foods Processing Applications**

24 Dielectric heating is one of the most promising alternatives to conventional thermal
25 treatment of fluid foods. The higher thermal efficiency and better heating uniformity of
26 radio frequency and microwave processes have been proven successful in providing a
27 similar or better bacterial and enzymatic inactivation in liquid and semi-solid foods while
28 improving the sensory and nutritional quality of the fresh product when compared to
29 conventional pasteurization. However, further investigations are necessary to advance
30 scaling up of applications at different frequencies and to better understand heat distribution
31 and energy consumption of industrial dielectric heating operations.

32 Keywords: dielectric heating, dielectric properties, liquid foods, microwave, radio
33 frequency

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46 **Introduction**

47 Thermal pasteurization and sterilization are fundamental operations in the processing of fluid
48 foodstuffs. They are widely used to destroy pathogenic and spoilage microorganisms, as well as
49 to inactivate enzymes responsible for quality deterioration during storage.^[1]

50 Conventional thermal processing (CP) of liquid and semi-solid foods is done by heat
51 exchangers, where the product flows while in indirect contact with a heating medium, usually hot
52 water, or steam. This operation has the disadvantage of causing over-heating near the tube
53 surfaces and requiring long heating times, which often compromises flavor, texture, and color of
54 the final product and causes loss of nutritional components.^[2]

55 In recent years, there is a growing consumer demand for sustainable, healthy, and high
56 quality products which should be shelf-stable but also possess the sensory and nutritional
57 qualities of the fresh product.^[1] Therefore, the development of less aggressive alternatives to
58 conventional thermal treatment is of great interest.^[3]

59 Dielectric heating has the potential to provide faster and more uniform heating rates,
60 while requiring less floor space and water input.^[4] In this technology, heat is created within the
61 material without the need for a temperature differential. This volumetric heating effect is not
62 possible with any other conventional mean and it reduces or eliminates the temperature
63 differences between external and internal layers, typical of conventional conduction mechanisms.
64 ^[5] Dielectric heating has been reported to possess higher efficiency in the electric consumption
65 and transformation into thermal energy when compared to convective heating.^[6]

66 Two different regions of the electromagnetic spectra are used in dielectric heating: Radio
67 frequency (RF) over a frequency range from 10 kHz to 300 MHz, and microwave (MW) over a
68 frequency range from 300 MHz to 300 GHz. Five frequencies have been allocated for industrial,

69 scientific and medical applications: 13.56, 27.12, and 40.68 MHz in the RF region and 915 and
70 2450 MHz in the MW region.^[7]

71 RF heating was first used in 1895 and it has a wide range of applications in the wood,
72 textile, paper, and cardboard industries. However, lack of research funding, lack of knowledge
73 among the equipment manufacturers and lack of general awareness of its potential advantages
74 have made their applications in the food industry not as prevalent as expected. Throughout the
75 years, its major uses in the food industry have been in defrosting and post-bake drying
76 processes.^[8, 9]

77 MW heating of food exists since 1949, and in recent decades it has become the norm in
78 domestic applications, changing food preferences and preparation methods. ^[10] However, further
79 understanding and optimization of the temperature distribution within the product is required for
80 industrial applications.^[11]

81 This review aims to address a revision about the advances of dielectric heating, with a
82 focus on its application on the thermal treatment of liquid foods and beverages. This paper is
83 divided in eight sections: Scientific principle, dielectric properties, applications, microbiological
84 considerations, nutritional aspects, sensory aspects, computational simulation and finally
85 combination of dielectric heating with other novel technologies.

86 **Scientific Principle**

87 Foods are usually materials with high content of water and other polar compounds. When
88 subjected to an external electric field, polar molecules in food behave like a dielectric in a
89 capacitor, orientating towards the direction of the applied field. This behavior is described by the
90 dielectric permittivity (ϵ) of the material. The intensity of the electric field is then reduced
91 relative to what it would be in free space by a factor of ϵ_r , which is the value of permittivity of a

92 given material divided by that of vacuum (ϵ_0):

$$93 \quad \epsilon_r = \frac{\epsilon}{\epsilon_0} \quad (1)$$

94 For air, relative permittivity is very close to 1. For foods, dielectric permittivity is the
95 main parameter that defines the electromagnetic energy absorption, reflection, transmission and
96 dissipation.^[12] In general terms, the dielectric activity of liquid foods is determined less by
97 physical structure like in solid matrices and more by the dielectric behavior of water molecules
98 and the mobility of solutes.^[13]

99 The response of materials to alternating electric fields such as those of electromagnetic
100 radiation is characterized by their complex permittivity:

$$101 \quad \epsilon^* = \epsilon' - j\epsilon'' \quad (2)$$

102 Where the real component ϵ' is often referred to as dielectric constant and is related to
103 energy storage, while the imaginary component ϵ'' is called the dielectric loss factor, which is
104 related to the thermal conversion.^[8] The values of dielectric constant and loss factor are
105 collectively referred to as the dielectric properties of the material.

106 In general terms, high moisture foods present a dielectric constant which decreases with
107 frequency, this is caused by a faster alternation of the electromagnetic field which makes it more
108 difficult for water molecules and clusters to orientate and polarize. Increasing temperature
109 increases the Brownian motion of the water molecules which reduces the energy storage.^[14]
110 Replacing water for less polarizable substances e.g. oil will also result in a reduced values of
111 ϵ' .^[15] In solid foods, adding salt can cause binding of water molecules reducing their
112 polarization, but this effect is often negligible in liquid foods.^[16]

113 Thermal conversion occurs by two main mechanisms: dipole relaxation and ionic
114 conduction. Therefore, the loss factor can be divided into its two main components as follows:

$$115 \quad \varepsilon'' = \varepsilon_{\sigma}'' + \varepsilon_d'' \quad (3)$$

116 Where ε_{σ}'' is the relative ionic loss and ε_d'' is the relative dipole loss.^[8]

117 Ionic loss occurs as a result of a net movement of dissolved ions in the direction of the
118 electric field, resulting in a higher macroscopic energy of movement and a subsequent rise in
119 temperature.^[17] Ionic conduction is the dominant dissipation mechanism at low frequencies,
120 decreasing linearly in a log-log plot against frequency. Ionic loss is directly proportional to ionic
121 conductivity, therefore, the loss factor increases with increasing temperature or salt
122 concentration.^[7, 16]

123 Dipole loss is caused by individual molecules of water and clusters of molecules aligning
124 themselves in the direction of the electric field. Clusters realign themselves with some delay, not
125 all energy is recovered and part of it is absorbed because of a net increase in molecular
126 movement. At high frequencies, dipole relaxation becomes the main loss mechanism, and it
127 increases at lower temperatures due to the relaxation times of water molecules approaching the
128 frequency of the applied electromagnetic field. If the frequency is too high, however, clusters will
129 not have enough time to rotate. The frequency at which the energy absorption capability by the
130 relaxation effect reaches a maximum, is called relaxation frequency.^[17]

131 Heating liquid foods causes a much higher increase in their loss factor compared to solid
132 matrices, since there is more ion mobility and viscosity effects.^[18] Figure 1 shows the
133 contribution of both loss mechanism at different frequencies and the effect of changes in
134 temperature.

135 Predictive models of heating rates and temperature distribution require knowledge of the
136 dielectric properties of the product. The amount of heat (provided to a material from
137 electromagnetic energy can be calculated from the value of loss factor as follows:

$$138 \quad P = 2\pi f \varepsilon_0 \varepsilon'' |\vec{E}|^2 \quad (4)$$

139 Where P is the power by volume unit, f is the frequency and E the local intensity of the
140 electric field, which is also dependent on the dielectric properties.^[19]

141 Power penetration depth of microwaves can be obtained from the dielectric properties of a
142 material and is applied in determining the dimensions of the food materials being processed.^[20]

$$143 \quad d_p = \frac{c}{2\pi f \sqrt{2\varepsilon' \left(\sqrt{1 + \left(\frac{\varepsilon''}{\varepsilon'}\right)^2} - 1 \right)}} \quad (5)$$

144 Where d_p is penetration deep, and c is the speed of light in vacuum. Penetration depth
145 can be described as the depth from the surface of the product at which the power density has
146 decreased 37 %, ^[21] or the microwave field has reduced to $1/e$. ^[22] The thickness of a liquid being
147 heated using dielectric heating should not exceed 2 or 3 times the penetration depth. ^[23] Since
148 penetration depth is inversely proportional to frequency, RF heating has the potential for better
149 heating uniformity than MW processes. ^[24]

150 **Measurement of the Dielectric Properties**

151 Accurate measurement of dielectric properties is of great importance in industrial applications, it
152 is essential in designing heating applicators, selecting optimal frequency ranges, formulating new
153 products and selecting package sizes and materials. ^[25] Not surprisingly, dielectric properties have

154 been extensively studied in fluid foodstuff such as fruit juices, sauces, purees, wine, honey, and
155 milk.

156 The most common method for the measurement of dielectric properties of liquid and
157 semi-liquids foods is the open-ended coaxial probe method. This method is based on the fact that
158 the phase and amplitude of the reflected signal on an open-ended coaxial line attached to a
159 material is dependent on its dielectric properties. The coaxial cable is connected to a network
160 analyzer which interprets the complex reflection coefficient of the sample to obtain the dielectric
161 properties in a determined frequency sweep. It is a non-invasive non-destructive method suitable
162 for a wide range of temperatures, however it is not suitable for small samples or materials of very
163 high permittivity.^[26]

164 Table 1 shows studies on the dielectric properties of liquid foods using the coaxial probe
165 method. It can be seen than most studies deal with temperatures below 100 °C, beyond this point
166 boiling of the sample can result in the formation of bubbles on the probe's surface, affecting the
167 measurement. However, during industrial heating processes, it is common to deal with
168 temperatures beyond the boiling point under pressurized conditions. Muñoz et al.^[27] dealt with
169 this limitation by using a pressurized vessel equipped with a heating jacket, managing to measure
170 the dielectric properties of milk at temperatures up to 150 °C.

171 Dielectric properties can be correlated with different parameters for use in quality control
172 of liquid foods. Zhu et al.^[28] developed models to relate the dielectric properties of raw milk with
173 the protein content, making it possible to develop a real-time, in-situ method for quality control
174 in the milk industry. Inokuchi et al.^[29] measured the dielectric properties of yogurt homogenized
175 with an air pump to obtain a method to analyze the content of air bubbles in yogurt. Guo et al.^[30]
176 measured the dielectric constant and loss factor of several honey-sucrose syrup mixtures to

177 evaluate its potential as a tool for detecting adulteration in honey. Guo et al.^[31] measured the
178 dielectric properties of cow's milk adulterated with water to obtain a frequency suitable to detect
179 adulteration. They also found a correlation between pH and loss factor, making it possible to
180 correlate it to the product's freshness. García et al.^[32] made daily measurements of the dielectric
181 properties of grape juice from 200 to 3000 MHz at 20 °C during its fermentation in the
182 production of red wine. They found that the adherence of CO₂ bubbles to the probe gave
183 unreliable measurements but that it could be useful to determine the extent of fermentation.

184 **Applications**

185 Dielectric heating technology has been successfully applied in several food products for
186 operations such as blanching, thawing, disinfesting, drying, baking, and cooking. Even with the
187 current limitations, some of these applications have found their way in the industry and are
188 currently applied in large-scale processes.^[24, 33]

189 Regarding liquid and semi-solid foods, recent research has focused on pasteurization and
190 sterilization, with fewer studies exploring the applicability in operations such as evaporation and
191 leaching. A number of successful MW technology applications can be found in literature for
192 liquid foods such as fruit juices,^[34-36] milk,^[37, 38] purees,^[39, 40] smoothies,^[3] sauces,^[41] sugarcane
193 juice,^[42] massecuite,^[43] creams,^[44] and peanut beverages.^[5] RF heating has been applied to liquid
194 foods to a much lesser extent, but its use has also been reported in milk,^[45] kiwi puree,^[46]
195 yogurt,^[47] fish soup,^[48] and liquid egg.^[49] For both technologies, the sensory and nutritional
196 quality, as well as the heating rates and associated inactivation kinetics have been investigated,
197 with emphasis on the comparison with CP treatments.

198 **Microbial Inactivation using Dielectric Heating**

199 Despite posing several advantages compared to CP of liquids and semi-solids, the industrial use
200 of dielectric heating for microbial inactivation is not as widespread as for other operations such as
201 dehydration, baking or thawing. One of the reasons is that there is still some lack of knowledge
202 about the kinetics of pathogen inactivation in foods during RF and MW exposure.^[39] Table 2
203 shows recent research aimed at better understanding this process.

204 Across the available literature, it is widely reported that dielectric heating technology
205 allows for higher inactivation efficiencies of pathogenic bacteria than CP. Qualitative tools to
206 predict inactivation levels during dielectric heating treatments have been developed for a number
207 of liquid foods and these models can even be associated to the dielectric properties of the raw
208 material. Kim et al.^[41] subjected samples of chili sauce with different sugar contents to heating at
209 1.5 and 3 kW in a 915 MHz microwave cavity applicator to evaluate the inactivation efficiency
210 on *E. coli* O157H7, *S. typhimurium* and *L. monocytogenes*. They found higher loss factor in
211 samples with less sugar content, which resulted in shorter times to reach the target temperature.
212 Authors also report that MW technology required a shorter time to achieve pathogen inactivation
213 than CP using a water bath.

214 The higher thermal efficiency observed in dielectric heating has resulted in claims of non-
215 thermal effects associated to this technology. The most predominant theories to explain this
216 phenomena were selective heating of microorganisms, electroporation, cell membrane rupture
217 and magnetic field coupling.^[50] Over the years, and with the development of more accurate
218 methods to record time-temperature history, non-thermal effects became harder to distinguish.
219 There is still controversial discussion taking place but currently, thermal effects are generally
220 considered the only cause of microorganism inactivation at industrial RF and MW frequencies.^[51]

221 Kou et al.^[51] suggest that claimed non-thermal effects were due to non-uniform
222 experimental temperature distributions with unprecise real-time temperature control. They
223 designed a *thermal death time* heating block to simulate the temperature-time curve obtained with
224 RF heating and compared the reduction of *E. coli* and *S. aureus* counts on apple juice and potato
225 puree with RF heating at 27.12 MHz, evaluating temperature uniformity and surface temperature.
226 After reaching same heating conditions, they found similar surviving patterns for both methods
227 and no statistical difference in bacterial inactivation.

228 Thermal treatments also have an important role as a mean of reducing the population of
229 spoilage microorganisms, allowing for an extended shelf life and an improvement of the sensory
230 properties of the product. Siefarth et al.^[47] applied a water bath RF heating system to reduce the
231 population of lactic acid bacteria and molds/yeasts in yoghurt to avoid post-acidification. They
232 evaluated three temperatures (58 °C, 65 °C and 72 °C) and applied CP using a convection oven
233 for comparison. They found microbial reductions for both treatments, showing a potential
234 increase in shelf-life. Furthermore, higher heating rates were obtained when using RF technology.

235 To evaluate the efficacy of a pasteurization process using a continuous-flow MW heating
236 system, Math et al.^[52] inoculated several blends of fruits and vegetables and evaluated the
237 reductions in yeasts/molds count, total aerobic count and *Enterobacteriaceae* after treatment and
238 during storage. Authors report total reduction of *Enterobacteriaceae* and yeasts/molds after
239 treatment, as well as satisfactory counts during storage. Cheng et al.^[53] determined the reduction
240 in total aerobic count of mandarin juice treated with MW at 90 °C for 70 s. They found > 2 log
241 reductions after processing. Lyu et al.^[46] compared the reduction in yeasts/molds and total
242 aerobic count of kiwi puree after non-continuous CP and RF treatments with the unpasteurized
243 product. They found no differences between treatments regarding yeasts/molds reduction.

244 Authors also report a retarded growth of total aerobic bacteria in RF samples during storage but
245 within acceptable limits.

246 Even if the presence of non-thermal effects has failed to be successfully proven in RF and
247 MW technology, the higher thermal efficiency and better temperature distribution in dielectric
248 heating operations have proven to allow for microbial reductions similar or higher than those of
249 CP processes.

250 **Nutritional Aspects**

251 High temperature processing can lead to degradation of thermolabile nutrients and volatile
252 compounds. The greater thermal efficiency of dielectric heating results in higher preservation of
253 thermosensitive compounds such as vitamin C, flavonoids, and anthocyanins.^[54] MW heating has
254 shown capacity to better retain bioactive compounds, often resulting in higher antioxidant
255 activity than the same product obtained by CP processes. In continuous-flow dielectric heating,
256 this effect is enhanced by lower tube surface temperatures and less overheating.^[1] Table 3
257 summarizes the related research in recent years.

258 Beneficial nutritional changes produced as a consequence of thermal treatments have also
259 been investigated for dielectric heating processes, Yu et al.^[55] found that during microwave
260 heating of tomato puree mixed with onion and olive oil, combinations of high power and short
261 heating time resulted in an increased lycopene isomerization and transfer into oil. Authors also
262 report that their recent data indicates higher proportion of Z-lycopene after microwave heating in
263 comparison with CP. Arjmandi et al.^[56] reported higher lycopene content increase in tomato,
264 carrot, pumpkin, and lemon smoothies after using continuous-flow MW treatment in comparison
265 with CP process, attributed to a higher cell-wall disruption. They also reported higher total

266 antioxidant capacity, total carotenoids content, total phenolics, total antioxidant capacity and
267 vitamin C.

268 Stratakos et al.^[57] were the firsts to compare MW and CP products by simulating
269 digestion with a model of epithelial tissue absorption combined with an in-vitro model. They
270 found a significantly higher cytoprotective effect of continuous-flow MW treated tomato juice
271 against H₂O₂ induced oxidation in human intestine cells, suggesting higher antioxidants content
272 in bioaccessible fractions.

273 In milk, microwave treatment has been reported to provide partial hydrolysis of proteins
274 into peptides with antihypertensive activity. Martins et al.^[54] analysed the antihypertensive
275 activity of microwave-treated orange juice milk beverages by measuring the angiotensin I-
276 converting enzyme inactivation, they found higher enzyme inhibition by treating with a lab-scale
277 MW digester in comparison with CP process using a heating mantle.

278 Current literature suggests that it is possible to enhance the nutritional properties of
279 thermally processed foods by making use of the higher thermal efficiency and better nutrient
280 extraction of dielectric heating technology. Food products of high nutritional value are, more than
281 ever, increasingly demanded by consumers. It is important to note that the nutritional value is
282 directly related to other quality parameters such as color, flavor, and stability during storage.

283 **Sensory Aspects**

284 ***Color***

285 According to Cheng et al.^[53] color is the main index for consumer's quality evaluation of fruit
286 and vegetable juices. Dielectric heating technology has been extensively reported to allow for
287 higher color retention after processing when compared to CP. This has been observed in products

288 such as kiwi puree,^[39] ^[46] strawberry puree,^[1] tomato puree,^[56] faba bean pesto sauce,^[58] and
289 mandarin juice.^[53] This phenomenon is generally attributed to a higher retention of pigments such
290 as anthocyanins, lycopene, carotenoids.

291 González-Monroy et al.^[59] compared the color of MW pasteurized tamarind beverages
292 with untreated samples, they found no statistical difference in any of the colorimetric coordinates.
293 These results are similar to those reported by Garnacho et al.^[60] on MW treated orange juice and
294 suggest a good color retention during the process. As stated before, faster heating rates and better
295 temperature uniformities translate to lower thermal degradation of pigments which in turn makes
296 it possible to better preserve the color of the fresh product.

297 Stratakos et al.^[57] found no difference in the color parameters of tomato juice treated with
298 continuous-flow MW and CP, possibly related to the fluctuations of the antioxidant capacity of
299 the samples during storage.

300 Surface overheating during continuous-flow heating of dairy products can cause Maillard
301 reactions which lead up to product browning and off-flavors. Reduced color changes after MW
302 treatment of dairy products has been observed in products such as milk^[61] and orange juice milk
303 beverages.^[54]

304 ***Flavor***

305 Heat treatments can lead to degradation or formation of components responsible for characteristic
306 flavors in fresh juices and purees, resulting in desirable or undesirable deviations from the fresh
307 product. ^[54] In this regard, profiling the volatile compounds and organic acids of different liquid
308 foods before and after dielectric heating processes has been subject of study in recent years.

309 Igual et al.^[62] compared the stability during 2 months of refrigerated storage of MW and
310 CP treated grapefruit juice. They found higher retention of citric acid after MW processing, and

311 no differences in malic acid or tartaric acid between treatments. Siguemoto et al.^[36] compared the
312 organic acid and volatile compound profile of continuous-flow MW and CP treatment of apple
313 juice with fresh juice. They found that the volatile profile of MW juice was closer to that of
314 untreated juice, they also found 1-heptanol exclusively in MW juice, which is associated with
315 leafy green and fresh notes. When comparing MW treated mandarin juice with CP and fresh
316 juice, Cheng et al.^[53] found a greater number of different aroma components and intermediate
317 concentrations in MW treated juice. Martins et al.^[54] found that orange juice milk beverages
318 treated with CP, had a higher number of volatile organic compounds than the fresh product, both
319 desirable and undesirable. The authors recommend MW technology at low temperatures since it
320 provided a profile of volatile organic compounds associated with a sweet and fruity aroma absent
321 in the fresh product.

322 In addition to the flavor compound profiling, sensory analysis has proven to be a powerful
323 tool to evaluate flavor changes associated to thermal treatments, helping to understand consumer
324 expectations on emerging technologies and what information affects their decisions.^[39] Better
325 acceptability scores after a dielectric heating process compared to CP have been reported in fish
326 soup,^[48] kiwi puree,^[39, 46] strawberry puree,^[1] apple puree,^[46] and faba bean pesto sauce.^[58]

327 Clare et al.^[61] compared milk treated by an indirect steam injection system with milk
328 treated with a continuous-flow MW heating unit over 12 months of storage using a descriptive
329 sensory analysis. They found that at all time points, MW milks had less brownish hues, less fatty
330 flavors, less astringency, and lower caramelized flavor.

331 ***Enzymatic inactivation***

332 Enzymatic inactivation is vital to ensure quality stability of fruit juices after a thermal treatment
333 and during storage. Polyphenol oxidase (PPO) and peroxidase (POD) are responsible for

334 discoloration and the development of off-flavors, pectin methyl esterase (PME) and
335 polygalacturonase (PG) destabilize the colloidal suspension of juices causing turbidity losses,
336 clarification and changes in the characteristic mouth feel. Table 4 shows recent research on
337 enzyme inactivation using dielectric heating technology.

338 Viscosity of semi-solid foods is associated to PME and PG inactivation since these
339 enzymes are responsible for pectin hydrolysis and changes in soluble pectin content. When
340 compared to CP treatment, Arjmandi et al.^[3] found higher viscosity in continuous-flow MW
341 treated vegetable smoothies, which also had the lowest residual activity of PME, PG and POD.
342 Zhou et al.^[63] found higher viscosity in defatted avocado puree after MW treatment. According to
343 the authors, this change provides a better mouthfeel in the product and is caused by an increase in
344 the soluble pectin content.

345 Enzyme inactivation can be used as a lethality reference for pasteurization treatments due
346 to their higher thermal resistance than most microorganisms. Lin et al.^[64] compared the alkaline
347 phosphatase activity in milk after continuous-flow MW heating and CP using a water bath. They
348 found faster inactivation using MW technology suggesting adequate pasteurization with a
349 reduced severity.

350 Some authors have suggested that microwaves might affect the non-covalent bonds of
351 polar or charged fractions of enzymes affecting their functionality in a different manner than
352 thermal treatments.^[65] However, this is not in accordance with some of the findings shown in
353 table 3. When performing comparison studies between CP and dielectric heating or other novel
354 technologies, it is important to maintain a strict control of the time-temperatures histories of the
355 samples, as well as the source of the enzymes. Regardless of this, the lower accumulated lethality

356 possible with RF and MW processes may facilitate the production of liquid and semi-solid foods
357 of enhanced overall quality.

358 **Computational Simulation of Continuous-flow Dielectric Heating Processes**

359 In the dielectric heating of liquids, convective heat transfer plays a major role in temperature
360 distribution. This makes possible to obtain a higher heating uniformity during continuous-flow
361 applications by adjusting pipe diameters, flow rates and system geometry.^[66] This convection
362 phenomenon, however, makes the predictive modeling of temperature profiles considerably more
363 challenging than in solid matrices, which is still one of the major limiting factors to the
364 popularization of this technology. Uneven temperature distributions can have a detrimental effect
365 on the quality of the product and compromise microbial safety.^[11]

366 With the growing calculation capacity of modern-day computers, more detailed
367 predictive-modelling of the distribution of electromagnetic energy during continuous-flow RF
368 and MW heating is becoming more accessible. The usual approach requires the simultaneous
369 solution of Maxwell's equation for electromagnetic field distribution, Navier-Stokes' equation
370 for conservation of momentum and Fourier's energy equation for electromagnetic power
371 absorbance and dispersion into heat. Knowledge of the temperature dependence of the dielectric
372 and thermal properties of the materials is therefore essential for accurate calculations.

373 Ratanadecho et al.^[67] were the first to investigate heating resulting from MW power
374 absorption on a liquid layer in a rectangular waveguide comparing it with experimental data.
375 They used finite difference time domain to develop a model including the electromagnetic,
376 hydrodynamic, and heat fields in two dimensions. They performed it on water and on a NaCl
377 solution, demonstrating the effect of dielectric properties on the heat distribution of liquids during
378 dielectric heating.

379 Zhu et al.^[68] used a similar approach to analyze forced convection in a liquid flowing
380 through a rectangular duct during MW heating of apple sauce, skim milk and tomato sauce. They
381 also analyzed the effect of applicator size and position within the MW cavity. Later, the same
382 authors would do a similar study in a circular pipe with a geometry that better resembled
383 industrial applications. They found that increasing pipe diameter increased power absorption up
384 to a critical diameter.^[69]

385 Cha-um et al.^[70] studied the dependence of temperature profile on MW power, waveguide
386 position, size and thickness of water and oil samples. Obtained results showed a good fit of the
387 model when compared to experimental data.

388 To make these calculations in a less computationally extensive way and obtain better
389 result visualization, Salvi et al.^[71] used COMSOL Multiphysics to obtain the temperature
390 distribution in water and in a carboxymethylcellulose solution during continuous MW heating
391 accounting for temperature dependent properties and phase change.

392 More recently, Tuta and Palazoğlu^[19] used a similar model with COMSOL Multiphysics
393 using water and carboxymethylcellulose but evaluating the effect of helical tubes to obtain
394 secondary flow and better temperature uniformity. From the Dean and Reynolds numbers, they
395 only found secondary flow in water but better temperature uniformity in both liquids due to the
396 microwaves entering from different surfaces in the coil. Zhang et al.^[72] expanded on this,
397 analyzing the effect of different structural parameters of helicoidal tubes on the heating efficiency
398 of the MW treatment. They conclude that parameters such as tube and pitch circle diameters
399 influence the extent of secondary flow and power distribution.

400 Kubo et al.^[11] prepared a model fruit juice using sucrose, citric acid, horseradish POD and
401 distilled water. They coupled enzyme inactivation kinetics with the electromagnetism, heat

402 transfer and fluid flow equations to investigate the validity of modelling lethality at each point of
403 the sample's volume and each instant of time. Authors conclude that other inactivation models
404 can be implemented with this approach, making it possible to correlate holding times and
405 incident energy to specific process targets.

406 Literature shows that temperature distribution during dielectric heating of fluid and semi-
407 solid foods can be predicted accurately if there is detailed knowledge of dielectric properties and
408 equipment dimensions. This information is critical to evaluate if sufficient heating rates can be
409 obtained for different products and different process parameters, allowing for a better process
410 control overall.

411 RF technology has the potential to provide even better temperature uniformity due to
412 much longer penetration depths; however, most of the available literature regarding predictive
413 modeling of RF processes deals with solid food matrices. Future years will probably see a
414 growing interest in computational modeling of dielectric heating operations to enhance
415 uniformity and to obtain spatial distributions for inactivation of enzymes and pathogenic
416 microorganisms.

417 **Combination of Dielectric Heating and other Technologies**

418 In recent years, there has been a growing interest in looking for possible synergistic effects
419 between dielectric heating and other new technologies. This line of research could lead to
420 overcoming the drawbacks of each individual process and achieve higher quality preservation
421 after treatment and during storage with less heat input.

422 Rayman and Baysal^[73] used electropulsation as a pre-treatment for MW and CP
423 processing of carrot juice pasteurization evaluating quality parameters after treatment and during

424 storage. They found higher phenolics content, carotenoids, PME inactivation and antioxidant
425 activity when combining electropulsation and MW compared to the control samples.

426 Zhang et al.^[74] processed kiwi fruit using RF technology combined with the addition of
427 nisin, a bacteriocin obtained from *Lactococcus lactis* subsp. *Lactis*. to reduce spores of different
428 strains of *Alicyclobacillus acidoterrestris* and *Alicyclobacillus contaminans*. They reported a
429 positive effect of RF treatment time, temperature, and nisin concentration on spore reduction.

430 Alvi et al.^[42] measured the antioxidant activity, evaporation rate, color, energy
431 consumption and solubility index of MW-assisted evaporated sugarcane juice at different power
432 levels. They found that evaporation rate increased, and antioxidant activity decreased for
433 increasing power levels. They also found a higher solubility index when compared to the juice
434 evaporated using the conventional process, which indicates a good reconstitution quality.

435 Das et al.^[75] used response surface methodology to optimize the treatment of bottle gourd
436 juice using MW and ultrasound technology. Response variables were *L. monocytogenes* cell
437 viability, and content of total phenolics, terpenoids and ascorbic acid. They found superior juice
438 quality parameters and higher bacterial inactivation when combining both technologies. When
439 compared to CP, they found higher antioxidant activity, vitamin content, higher protein content
440 and less color change.

441 To produce a shelf-stable milk with improved nutritional and sensory qualities, Graf et
442 al.^[76] developed a process to separate skim milk into two fractions using microfiltration, and
443 subsequently treat each of them using CP or MW heating according to their constituents.

444 Finally, there is recent literature focused on the use of dielectric technology to assist
445 operations not related to pasteurization. Chua and Leong^[77] studied the effect of sample size and
446 evaporation rate on the quality parameters of concentrated pineapple juice obtained by MW

447 assisted evaporation. They found low activity of proteolytic enzymes and low browning at high
448 mass evaporation rates, associated with longer MW heating times.

449 Yu et al.^[78] used MW technology and ultrasound in the leaching of jujube juice and
450 compared it with conventional leaching. They found higher total soluble solids, higher soluble
451 pectin, less protopectin, higher galacturonic acid and less pectinase activities applying ultrasound
452 before MW.

453 When comparing rotary evaporation of orange juice with MW vacuum evaporation at
454 different pressures, Bozkir^[79] found higher evaporation rates in the latter, accompanied by
455 smaller color changes and lower degradation rates of vitamin C, total phenolics and total
456 carotenoids.

457 **Future Trends and Prospective**

458 Over the past 10 years, the effect of dielectric heating on microbial reduction, enzyme
459 inactivation and preservation of nutritional and sensory quality of liquid and semi-solid foods has
460 been extensively investigated. Comparison with conventional thermal treatments have shown that
461 it is possible to obtain a shelf-stable, high-quality product in compliance with food safety
462 regulations. To widen the field of applications of dielectric heating technology in liquid foods,
463 there is scope for improvement in the following areas:

- 464 • Increasing the available data on the dielectric properties of different liquid foods, with
465 special emphasis on temperatures above the boiling point under pressurized conditions.
- 466 • Further advancing temperature profile mathematical modelling, specially of RF heating
467 applications since it is currently limited to solid foodstuffs.

- 468 • Expanding the current research to 13.56, 40.68, and 915 MHz, frequencies which have
469 been investigated to a lesser extent and could offer advantages in diverse applications.
- 470 • Advancing the scaling-up of dielectric heating applicators of novel geometric design,
471 accompanied by an evaluation of resource use and environmental impact.
- 472 • Further investigations about the possible synergistic effects of MW and RF heating with
473 other technologies to overcome the current limitations.
- 474 • Correlate heat generation in fluid products with energy consumption in order to optimize
475 heating process.
- 476 • Develop simple life cycle assessment decision support tools to conduct dielectric heating
477 process

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482 **Declaration of Interests Statement**

483 The authors report there are no competing interests to declare.

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805 **Tables**

806 Table 1. Selected studies on dielectric properties of liquid and semi-solid foods.

Material	Frequencies	Temperature	References
Soy sauce	300-3000 MHz	5-70 °C	[22]
Milk, soy beverages, pudding and avocado paste	915 MHz	10-90 °C	[18]
<i>Salsa con queso</i>	915 MHz	20-130 °C	[80]
Mirin	300-3000 MHz	5-70 °C	[81]
Peanut beverages	915 MHz	18-90 °C	[5]
Vinegar and acetic acid solutions of different concentration	1-20 GHz	20-22 °C	[82]
Yellow locust flower honey, jujube flower honey and rape flower honey	10-4500 MHz	25 °C	[83]
Apple, orange, pear, grape and pineapple juice	20-2400 MHz	15-95 °C	[25]
Homogenate of different tomato tissues, with different concentrations of NaCl and CaCl ₂	300-3000 MHz	22-120 °C	[16]
Cow and Goat milk	10-4500 MHz	25-75 °C	[37]
Green coconut water	500-3000 MHz	0-90 °C	[14]
Simulated solutions of salt and sugar from green coconut water			
Citrus fruit juices and their blends	500-3000 MHz	0-90 °C	[34]
Model juice solutions and apple, pineapple and orange juices	200-3000 MHz	20-80 °C	[84]
Raw and packed soy milk formulations	500-20000 MHz	20-70 °C	[85]
Raw milk, skimmed milk, 35 % concentrated non fat milk	10-2450 MHz	20-150 °C	[27]
Tomato, salt and olive oil homogenates	10-3000 MHz	10-100 °C	[86]

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808 Table 2. Selected studies on RF and MW pasteurization of liquid and semi-solid foods.

Product	System	Frequency (MHz)	Power (W)	Species	Reduction (log UFC/mL)	Processing conditions	References
Milk	Continuous-flow 50 Ω RF applicator	27.12	1200	<i>L. innocua</i>	>4.69	Residence time: 55.5 s	[45]
				<i>E. coli</i> K-12	>7	Outlet temperature: 65 °C	
Sweet potato puree	Continuous-flow, two applicator MW system at 915 MHz	915	60000	Plastic pouches bioindicators of <i>B. subtilis</i> , <i>G. stearothermophilus</i>	>4.69 for <i>B. subtilis</i> , >4.26 for <i>G. stearothermophilus</i> 132 °C and 138 °C	Residence time: 25 s Temperatures: 126 °C 132 °C 138 °C	[40]
Mango juice	MW oven with refractory glass spirals for continuous-flow	2450	1500	<i>Aspergillus. spp.</i>	1	Max. temperature: 52 °C	[87]
Apple puree	MW oven	2450	652	<i>E. coli</i> O157:H7	1.01	Treatment time: 35s	[88]
				<i>L. innocua</i>	>2.82	Max. temperature: 75.3 °C	

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812 Table 2. (Continued)

Product	System	Frequency (MHz)	Power (W)	Species	Reduction (log UFC/mL)	Processing conditions	References
Asparagus cream	MW oven	2450	720, 810, 900	<i>A. acidoterrestris</i>	2 for t= 5 min at 900 W, t= 6 min at 810 W, t= 7 min at 720 W	Treatment time: 3-7 min	[44]
Kiwi puree	MW oven	2450	600, 900, 1000	<i>L. monocytogenes</i>	>5 for t>75 s at 900 W and t>82 s at 1000 W	Treatment time: 50-340 s	[39]
Reconstituted powder instant formula milk	MW oven	2450	400, 500, 600, 700, 800, 900	<i>Cronobacter sakazakii</i>	>5 for 120 min at 700, 800 and 900 W	Treatment time: 30-120 s	[38]
Salsa	WR-975 Waveguide MW system with turntable and stirrer	915	1200, 1800, 2400, 3600, 4800	<i>S. Typhimurium</i> <i>L. monocytogenes</i> , <i>E. coli</i> O157:H7	5.76-6.10 4.51-4.84 5.17-6.21	Final temperature: 90 °C	[89]

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815 Table 2. (Continued)

Product	System	Frequency (MHz)	Power (W)	Species	Reduction (log UFC/mL)	Processing conditions	References
Tomato puree	MW oven	2450	950	<i>E. coli</i> O157:H7	4.88	Treatment time: 3 min	[90]
Apple juice	Adapted MW oven	2450	400, 600, 800, 1000	<i>E. coli</i> O157:H7 <i>L. monocytogenes</i>	>5 >5 At 1000 W	Treatment time: 110 s for <i>E. coli</i> 130 s for <i>L. monocytogenes</i>	[91]
Cantaloupe juice	MW oven	2450	400, 800	<i>E. coli</i> O157:H7 <i>S. aureus</i> <i>S. enterica</i> serovar Enteritidis <i>S. Typhimurium</i>	>8 for 110 s for all microorganisms	Treatment time: Up to 110 s Inactivation started from 50 s	[92]
Apple juice	MW oven	2450	720, 600	<i>E. coli</i> O157:H7 <i>S. Typhimurium</i>	>5	Treatment time: > 20 s for 720 W > 25 s for 600 W	[35]
Liquid whole egg, liquid egg white, liquid egg yolk	Parallel electrode free running RF unit	27.12	1200	<i>S. enterica</i> serovar Enteritidis	5.62 4.36 5.31	Treatment time: 220 s 285 s 180 s At different electrode gaps	[49]

816 Table 3. Selected studies on nutritional properties of liquid and semi-solid foods treated with dielectric heating.

Product	Dielectric heating conditions	Conventional heating conditions	Significant findings on nutritional properties	References
Grapefruit juice	MW Oven	Water bath	Similar reduction of antioxidant capacity for both processes	[62]
	900 W 30 s	80 °C 11 s	Higher ascorbic acid retention in MW process and during storage	
Kiwi puree	MW oven	Stainless steel batch retort	No change in total tannins after processing	[39]
	1000 W 340 s	84 °C 300 s	Higher reduction of total flavonoid and phenol content, and vitamins A, C, and E after CP process	
Strawberry puree	Continuous-flow MW	Gas-heated bath pasteurizer	Higher degradation of polyphenols, anthocyanins, and vitamin C in CP	[1]
	2450 MHz 20000W	90 °C 15 min		
	90 and 120 °C for 10 s 80 and 90 °C for 7 s			
Tomato puree	Continuous-flow MW	Thermomix	No differences in total phenolics content	[93]
	96 °C 35 s	96 °C 35 s	Greater reduction in antioxidant capacity and vitamin C in CP	
	Different combinations of power and time		More enhancement of lycopene extraction and higher β -carotene content after thermal treatment, especially for high power/short time MW process	

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820 Table 3. (Continued)

Product	Dielectric heating conditions	Conventional heating conditions	Significant findings on nutritional properties	References
Pomelo Juice	MW oven	Water bath	Higher reduction in ascorbic acid and total phenolics content in CP	[94]
	90 °C	90 °C 15 s	Higher reduction of tannin and naringin in MW heating	
Kiwi puree	RF System, time: 210 s	Water bath	Higher antioxidant capacity and retention of phenolic compounds and ascorbic acid in RF treatment	[46]
	10000 W, 27.12 MHz	90 °C		
	Electrode gap: 105 mm	60 s		
Faba bean pesto sauce	Semi-industrial semi-continuous MW oven	Table-top food processor	Higher carotenoid content in MW compared to CP	[58]
	2450 MHz, 11 kW	85 °C 5 min	Reduction of tannins after processing only in MW	
	85 °C 30 s		Higher phenolic content in MW compared to CP No difference in antioxidant capacity between MW and CP	
Apple juice	Continuous-flow MW	Counter-current coil heat exchangers	Increase in phenolic compounds and antioxidant capacity of both thermal treatments compared to untreated juice	[36]
	6000 W, 2450 MHz			
	70, 80, 90 °C	70, 80, 90 °C		

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825 Table 3. (Continued)

Product	Dielectric heating conditions	Conventional heating conditions	Significant findings on nutritional properties	References
Cantaloupe juice	MW oven 400 W, 800 W Time: 110s	Water bath 27-75 °C 30 min	Higher loss of vitamin C, but lower loss of β -carotene and phenolic compounds compared to CP	[92]
Camu-camu juice	MW oven 2450 MHz 310, 625, 940 W 15, 30, 45 s	Heating bath 85 °C 60 s	Ascorbic acid content increased after MW and decreased after CP when compared to untreated samples	[95]
Mandarin juice	MW oven 800 W, 90 °C Time: 70 s	Water bath 90 °C 30 s	Less reduction of ascorbic acid, higher carotenoid content, and more retention of phenolic compounds compared to CP	[53]

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832 Table 4. Select studies on enzyme inactivation during dielectric heating of liquid and semi-solid foods.

Product	Dielectric heating conditions	Conventional heating conditions	Significant findings on enzymatic inactivation	References
Grapefruit juice	MW Oven 900 W 30 s	Water bath 80 °C 11 s	Higher degree of POD inactivation in CP treated grapefruit juice compared to MW. Residual PME activity after both processes but within range of acceptability.	[62]
Kiwi puree	MW oven 1000 W 340 s	Stainless steel batch retort 84 °C 300 s	Both treatments inactivated 90 % of PPO, used as indicator. MW was more effective at inactivating PPO and PME than CP.	[96]
Strawberry puree	Continuous-flow MW 2450 MHz 20000W 90 and 120 °C for 10 s 80 and 90 °C for 7 s	Gas-heated bath pasteurizer 90 °C 15 min	Higher inactivation of PPO and POD in the CP treatment. POD showed lower resistance to MW heating than PPO. Best compromise between enzyme inactivation, color, and nutrient preservation for MW treatment at 90 °C.	[1]
Orange juice	MW synthesis reactor 2450 MHz 300 W 50-90 °C 0-60 s	Polyethylene rectangular packages in a water bath 50-95 °C 0-60 s	A model two-fraction PME inactivation model was obtained. Better inactivation efficiency using MW Only MW reached 90 % inactivation at 60 s.	[97]

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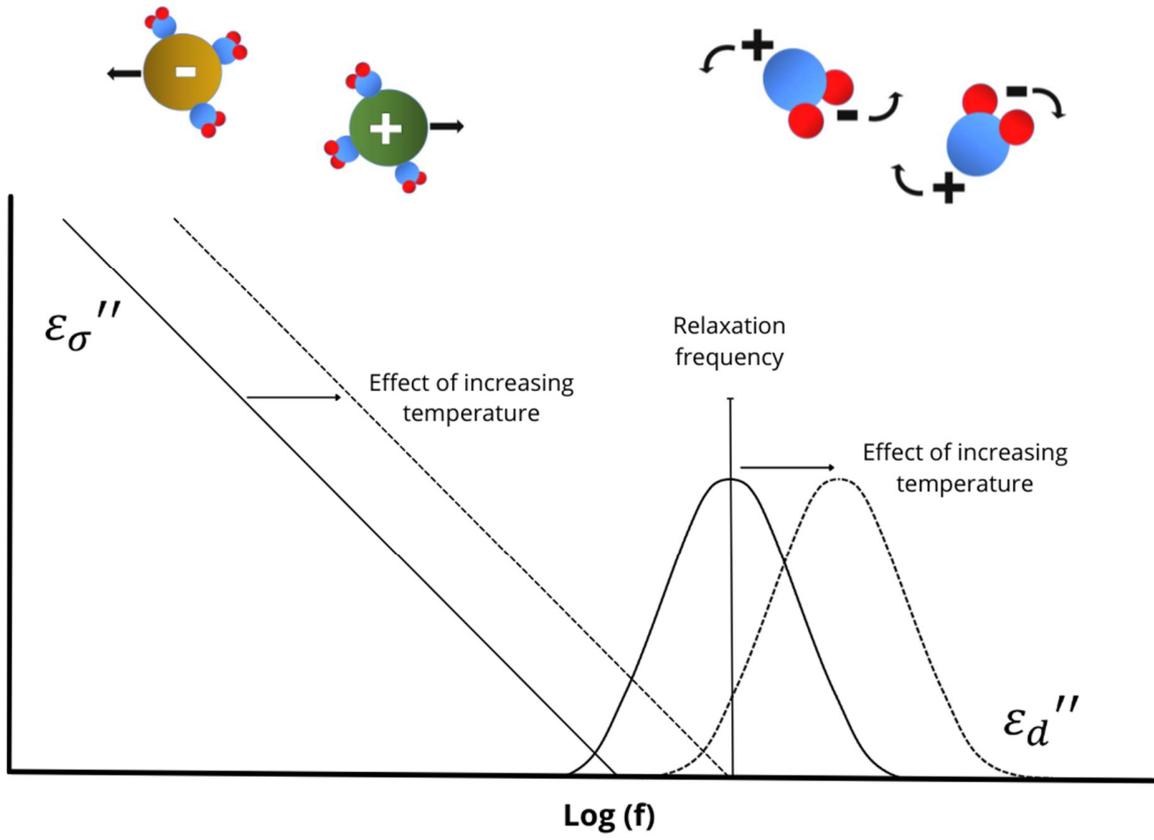
835

836 Table 4. (Continued)

Product	Dielectric heating conditions	Conventional heating conditions	Significant findings on enzymatic inactivation	References
Apple juice	MW reactor 2450 MHz 300 W 50-90 °C 20-270 s	Polyethylene pouches inside water bath 50-90 °C 20-270 s	A model two-fraction PME inactivation model was obtained. No evidence of non-thermal effects was found in the inactivation kinetics of PME, POD and PPO.	[2]
Apple juice	Continuous-flow MW 70, 80, 90 °C 0.4-0.9 L/min	Heat exchanger 70, 80, 90 °C 0.4-0.9 L/min	Enzymatic residual activities from measured temperatures and residence times along the path were predicted. MW process was closer to the ideal instantaneous heating/cooling conditions, allowing for a more efficient enzyme inactivation.	[98]
Camu-camu juice	MW oven 2450 MHz 310, 625, 940 W 15, 30, 45 s	Heating bath 85 °C 60 s	Only 940 W showed lower activity of POD compared to CP Only 310 W/15 s showed higher activity of PPO compared to CP	[95]

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838 Figures



848 **Figure Captions**

849 Figure 1. Contribution of ionic conduction and dipole relaxation to the overall loss factor of
850 materials as function of frequency.

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